

## SHORT COMMUNICATION

# CH<sub>4</sub> Decomposition to Green H<sub>2</sub> over PM(1wt%)-Ni(20wt%)/MCM-41 (PM = Pd, Pt, and Rh) Catalysts

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## ABSTRACT

The CH<sub>4</sub> is a greenhouse gas with a global warming potential(GWP) 21 times greater than CO<sub>2</sub>. The catalytic decomposition of CH<sub>4</sub> (CDM) is a climate-friendly, CO<sub>2</sub>-free process that produces only green H<sub>2</sub> and carbon nanomaterials such as carbon nanotubes. The CDM to green H<sub>2</sub> over PM(1wt%)-Ni(20wt%)/MCM-41 (PM = Pd, Pt, and Rh) catalysts was investigated using a packed-bed flow reactor(PBFR) under atmospheric pressure. The catalysts were characterized through XPS and XRD. XRD analysis revealed that NiPd crystallites were formed owing to appropriate interactions between Ni<sup>2+</sup> and Pd<sup>2+</sup>. XPS analysis revealed that adding of 1 wt% of Pd to Ni(20wt%)/MCM-41 increased the Ni2p atomic percentage of Pd(1wt%)-Ni(20wt%)/MCM-41 from 2.77% to 4.27%, and decreased that of O1s the from 68.59% to 66.92%. The core electron levels, such as Ni2p, O1s, and Si2p in fresh Pd(1)-Ni(20)/MCM had a slight chemical shift toward lower energy compared to those of Ni(20wt%)/MCM-41. The H<sub>2</sub> yield on the Pd(1 wt%)-Ni(20wt%)/MCM-41 is much higher than that of PM(1wt%)-Ni(20wt%)/MCM-41 (PM = Pt, Rh) and Ni(20wt%)/MCM-41 even after  $1.2 \times 10^4$  s of CDM, while that of Ni(20wt%)/MCM-41 decreased rapidly. The H<sub>2</sub> yield of Pd(1wt%)-Ni(20wt%)/MCM-41 in CDM was enhanced owing to the increased Ni2p distribution and the enhanced reduction degree caused by H<sub>2</sub> spillover via appropriate metal-carrier interaction (AMCI) between Pd, Ni, and MCM-41. The CDM is an environmentally friendly process that produces CO<sub>x</sub>-free and economical green H<sub>2</sub> by using a catalyst of 1 wt% Pd onto Ni(20wt%)/MCM-41.

**Keywords:** Green H<sub>2</sub>; Global Warming Mitigation; Climate Change; Clean Energy; CH<sub>4</sub> Decomposition

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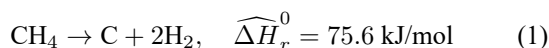
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# 1. Introduction

As the concentration of CH<sub>4</sub> in the atmosphere increases owing to human activities such as the use of fossil fuels, agriculture, and landfills, climate change is changing, seriously affecting the global environment such as weather phenomena, rising sea levels, and changes in marine ecosystems. The IPCC report<sup>[1]</sup> emphasizes that carbon neutrality requires a strong reduction in not only carbon dioxide but also other greenhouse gas emissions such as CH<sub>4</sub>. The CDM has attracted significant attention as a promising alternative for climate-friendly green H<sub>2</sub> without greenhouse gas emissions, such as CO<sub>x</sub> and NO<sub>x</sub><sup>[2]</sup>. On the other hand, the steam reforming (SMR) and partial oxidation of CH<sub>4</sub> (POM) to grey H<sub>2</sub> emit a lot of greenhouse gases, namely CO<sub>x</sub>, CO and CO<sub>2</sub>, which have a serious greenhouse effect on the Earth. The CH<sub>4</sub> is a greenhouse gas with a GWP<sup>[3]</sup> 21 times greater than CO<sub>2</sub>. Also, the CH<sub>4</sub> is the main component of natural gas and is endothermic, as shown in equation (1). It only produces green H<sub>2</sub> and nanocarbon materials without emitting CO<sub>x</sub>. However, the implementation of CDM is challenging owing to its energy-intensity and thermodynamic tendency toward carbon deposition, which causes catalyst deactivation.



The precious metals, such as palladium, platinum, and rhodium are effective in maintaining high activity and stability in CDM, but they are unsuitable owing to high cost and scarcity in terms of industry. Using group VIII 3d transition metal, nickel(Ni) offers an industrially viable alternative, providing both low cost and high availability<sup>[4, 5]</sup>. It exhibits excellent initial catalytic activity but is prone to rapid carbon deposition on the catalyst surface, leading to catalyst deactivation. Various strategies have been explored to extend the lifespan of Ni catalysts and mitigate carbon deposition on the catalyst surface<sup>[6]</sup>. Takriff et al.<sup>[7]</sup> report that adding Pt to Ni/CeO<sub>2</sub> enhances the activity and stability in CDM reaction by lowering the NiO reduction temperature through H<sub>2</sub> spillover while improving the uniform distribution of fine particles on the catalyst through moderate metal-carrier interaction. Dai et al.<sup>[8]</sup> report that the appropriate addition of precious metal promoters such as Pd, Pt, and La to a Ni-based catalyst in CDM for H<sub>2</sub> increases catalyst activity and

prevents carbon deposition on the catalyst. Millar et al.<sup>[9]</sup> report that MCM-41, with pore sizes ranging from 2 nm to 50 nm in a uniform hexagonal structure, is widely used as a catalyst carrier and adsorbent because of its physical properties, including thick walls and high thermal stability.

This study aims to investigate the effect of platinum-group metals(PM)(Pd, Pt, and Rh) as promoters to develop a catalyst with sustained high activity and long-term stability. In terms of economic feasibility and efficiency for producing green H<sub>2</sub> under CDM. The catalysts used were characterized by X-ray Photoelectron Spectroscopy (XPS) and X-ray Diffraction(XRD). They evaluated through catalyst performance tests in CDM using a PBFR under atmospheric pressure for green H<sub>2</sub>.

## 2. Materials and Methods

### 2.1. Catalyst Preparation

PM(1wt%)-Ni(20wt%)/MCM-41 (PM = Pd, Pt, and Rh) catalysts were prepared using a standard support method. Ethanol(99.9%, Daejung, South Korea) was added to the reactor, followed by dissolving  $2.0 \times 10^{-6}$  kg each of Pd(NO<sub>3</sub>)<sub>2</sub>·xH<sub>2</sub>O(Aldrich), Pt(NO<sub>3</sub>)<sub>2</sub>·xH<sub>2</sub>O(Aldrich), Rh(NO<sub>3</sub>)<sub>2</sub>·xH<sub>2</sub>O(Aldrich), alongside  $3.0 \times 10^{-4}$  kg of Ni(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O(Aldrich) in ethanol. Subsequently,  $1.0 \times 10^{-4}$  kg of MCM-41 (Aldrich) was added, and the mixture was stirred uniformly for  $1.8 \times 10^4$  s. The resulting precipitate was filtered and dried in a dryer at 373K for  $8.6 \times 10^4$  s. The dried sample was calcined at 773 K for  $1.8 \times 10^4$  s in an electric furnace (Eyela, TMF-1000) to create PM(1wt%)-Ni(20wt%)/MCM-41 (PM = Pd, Pt, and Rh), Ni(20wt%)/MCM-41, and Pt(1 wt%)/MCM-41 catalyst. The calcined sample was then ground to 150–200 mesh for use.

### 2.2. Catalyst Characterization

XRD pattern was obtained using a Panalytical Empyrean 3D high-resolution X-ray diffractometer with Cu K $\alpha$  radiation( $\lambda = 1.5419 \text{ \AA}$ ; 40 kV, 30 mA). XPS Spectra were acquired using Alk $\alpha$  X-rays under operating conditions of  $1 \times 10^{-9}$  mbar and 1.75 keV with an HP-X-ray photoelectron spectrometer (Thermo Scientific K-Alpha+).

## 2.3. Catalyst Performance

The CDM to H<sub>2</sub> was performed using a PBFR under atmospheric pressure with process stability and energy reduction effects. A  $5.0 \times 10^{-5}$  kg of powdered catalyst was placed on quartz cotton within a quartz reactor with a  $1.0 \times 10^{-2}$  m internal diameter and 0.3 m length. Subsequently, pure CH<sub>4</sub> (99.999%, Samjung Co., South Korea) was supplied to the reactor at a gas hourly space velocity (GHSV) of  $1.2 \times 10^{-2}$  CH<sub>4</sub> mL/kg<sub>cat.</sub>·s under reaction conditions of 973K and 101.3 kPa. The reactor temperature was controlled within  $\pm 1$ K using a PID controller with a K-type thermocouple placed on the catalyst in the reactor. After purging the reactant through a pressure gauge attached to each cylinder, the reactant composition was regulated with a mass flow controller (Aalborg, USA). The product was analyzed using a thermal conductivity detector with a Molecular sieve 5 A column connected to a Gas chromatograph (Shimadzu Co., Model 14B, Japan). Before the reaction, the catalyst was employed by reducing the H<sub>2</sub> temperature to 773 K for  $1.8 \times 10^4$  s at  $3.3 \times 10^{-1}$  ml/s flow rate, then increasing the reaction temperature at a rate of 4.7 K/s. The data were used as an average value obtained by performing three to five experiments. The H<sub>2</sub> yield for each catalyst was calculated using the following equation:

$$\text{H}_2 \text{ yield (\%)} = \frac{\text{moles of H}_2 \text{ produced}}{2 \times \text{moles of CH}_4 \text{ in the feed}} \times 100 \quad (2)$$

## 3. Results and Discussion

### 3.1. Catalyst Activity

**Figure 1** illustrates the H<sub>2</sub> yield vs. reaction time for CDM over the PM(1wt%)-Ni(20wt%)/MCM-41 (PM = Pd, Pt, and Rh), Ni(20wt%)/MCM-41, and Pt(1)/MCM-41 catalysts. The H<sub>2</sub> yield for the Pd(1wt%)-Ni(20wt%)/MCM-41 catalyst remained relatively constant, averaging approximately 62.1%. However, the H<sub>2</sub> yield for the Rh(1 wt%)-Ni(20wt%)/MCM-41 catalyst initially stabilized, reaching about averagely at approximately 60.8% but declined rapidly, reaching 23.6% at  $1.6 \times 10^4$  s. The H<sub>2</sub> yield for the Pt(1wt%)-Ni(20wt%)/MCM-41 catalyst was initially lower than that of the Ni(20wt%)/MCM-41 catalyst until  $8.3 \times 10^3$  s; however, after that, the Pt(1wt%)-Ni(20wt%)/MCM-41 catalyst showed a significantly higher H<sub>2</sub> yield than that of the Ni(20wt%)/MCM-41 catalyst. Moreover, the H<sub>2</sub> yield

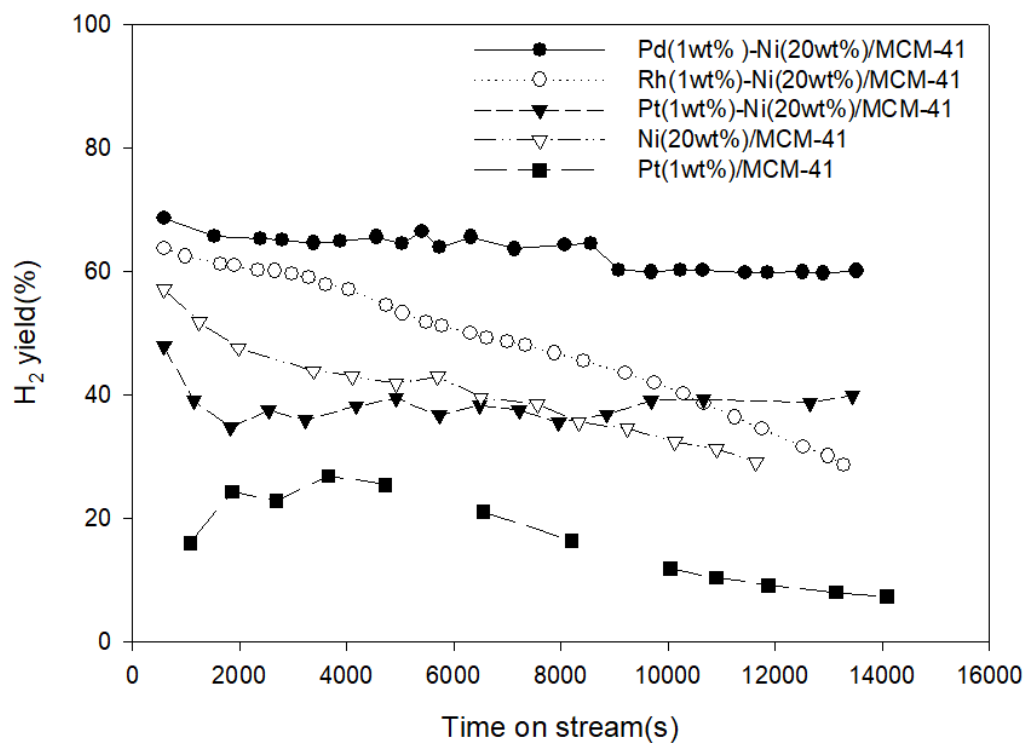
for the Ni(20wt%)/MCM-41 catalyst decreased continuously, reaching 29.1% at  $1.2 \times 10^4$  s. Additionally, the H<sub>2</sub> yield for Pt(1wt%)/MCM-41 catalyst continued to increase until  $2.7 \times 10^3$  s, reaching 55.2%, but decreased rapidly after that, dropping to 22.3% at  $1.7 \times 10^4$  s.

This phenomenon is owing to a lot of carbon deposition<sup>[10]</sup> on the Ni(20wt%)/MCM-41 catalyst surface and sintering of Ni particles caused by the low Tammann temperature. The addition of 1 wt% PM (Pd, Pt, and Rh) as a promoter to Ni(20wt%)/MCM significantly affected the H<sub>2</sub> yield of CDM. The H<sub>2</sub> yield of Pd(1wt%)-Ni(20wt%)/MCM-41 was approximately 1.5 times higher than that of Ni(20wt%)/MCM-41. The H<sub>2</sub> yield of the catalysts used in CDM at  $1.2 \times 10^4$  s followed the order — Pd(1wt%)-Ni(20wt%)/MCM-41  $\gg$  Pt(1wt%)-Ni(20wt%)/MCM-41  $>$  Rh(1wt%)-Ni(20wt%)/MCM-41  $>$  Ni(20wt%)/MCM-41  $\gg$  Pt(1 wt%)/MCM-41. The H<sub>2</sub> yield is assumed to be improved by Ni2p distribution<sup>[7]</sup> owing to appropriate metal-carrier interactions among the PM (Pd, Pt, and Rh), Ni, and MCM-41 alongside increased reduction degree, which causes H<sub>2</sub> spillover<sup>[11]</sup>. Otsuka et al.<sup>[12]</sup> reported that CDM was performed on an M-Ni (5 wt%) (M = Pd, Pt, Rh) catalyst at a reaction temperature of 823 K and an M/Ni molar ratio of 0.1, and that adding Rh and Pt to Ni (5 wt%)/SiO<sub>2</sub> shortened the catalyst life, but adding Pd improved it. Economical green H<sub>2</sub> can be produced by using catalyst of 1 wt% Pd onto Ni(20wt%)/MCM-41 in the CDM process.

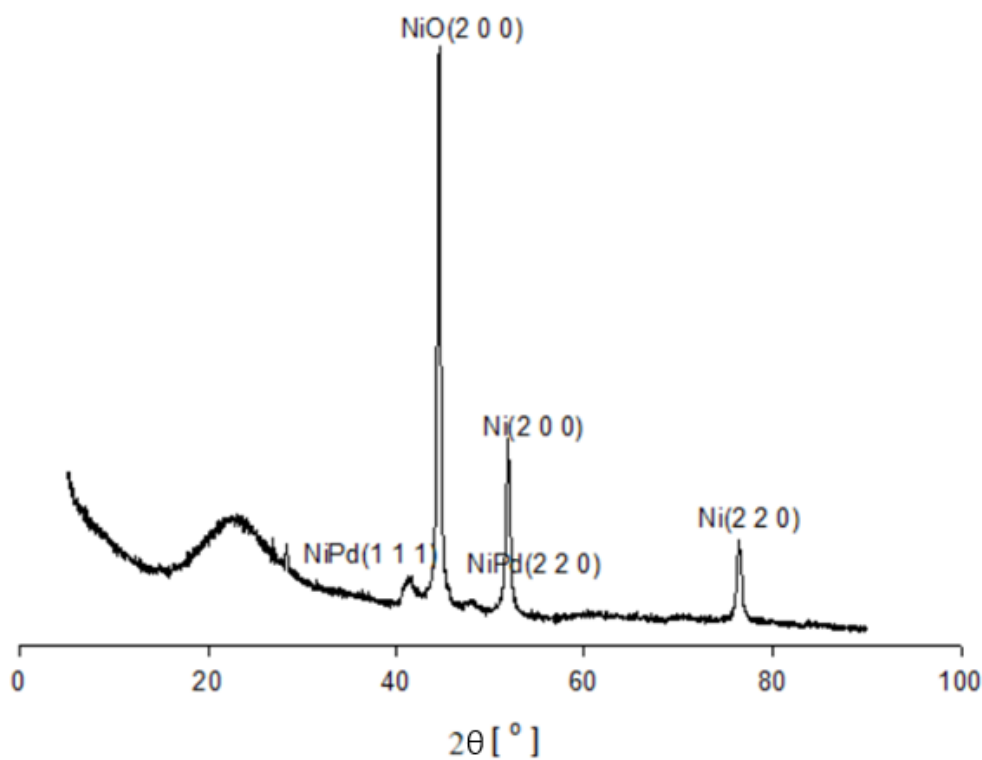
### 3.2. Characterization of Fresh Pd(1wt%)-Ni(20wt%)/MCM-41 Catalyst

**Figure 2** displays the XRD patterns of fresh Pd(1wt%)-Ni(20wt%)/MCM-41 catalyst reduced before reaction. Characteristic peaks of NiO at  $2\theta = 44.53^\circ$  and them of cubic Ni were observed at  $2\theta = 51.89^\circ$  and  $76.38^\circ$ , showed the presence of NiO(2 0 0)<sup>[6]</sup>, Ni(2 0 0), Ni(2 2 0) planes (JCPDS: 03-1051), respectively, alongside those of cubic NiPd at  $2\theta = 41.69^\circ$ ,  $45.18^\circ$ , showed the presence of NiPd(1 1 1), NiPd(2 2 0) planes<sup>[13]</sup>, respectively. However, no characteristic peaks for Pd were detected. These results suggest the NiPd crystallites formation, indicating an appropriate interaction between Ni<sup>2+</sup> and Pd<sup>2+</sup>.

It is believed that the NiPd crystalline phase will affect high H<sub>2</sub> yield and catalyst stability<sup>[13]</sup>.



**Figure 1.**  $H_2$  yield from  $CH_4$  decomposition over PM(1wt%)-Ni(20wt%)/MCM-41 (PM = Pd, Pt, and Rh), Ni(20wt%)/MCM-41, and Pt(1wt%)/MCM-41 in a PBFR under the following conditions:  $P = 101.3$  kPa,  $T = 973$  K, and  $GHSV = 1.2 \times 10^{-2} CH_4$  mL  $kg_{cat}^{-1} s^{-1}$ .



**Figure 2.** Standard XRD patterns of fresh Pd(1wt%)-Ni(20wt%)/MCM-41.

**Table 1** presents the atomic percentage of core electron levels for fresh Pd(1wt%)-Ni(20wt%)/MCM-41 and Ni(20wt%)/MCM-41 catalyst reduced before reaction, as determined via XPS. The addition of 1 wt% of Pd to the Ni(20wt%)/MCM-41 catalyst increases the atomic percentage of Ni2p from 2.77% to 4.27%, while that of O1s decreases from 68.59% to 66.92%. The 1.50% increase in Ni2p atomicity on Pd(1wt%)-Ni(20wt%)/MCM-41 surface is attributed to the appropriate metal-support interaction among Ni, Pd, and MCM-41, indicating high dispersion of Ni particles. The atomic percentage of O1s core electron

levels, including lattice oxygen and oxygen vacancies of the Pd(1wt%)-Ni(20wt%)/MCM-41 was 1.02 times lower than that of the Ni(20wt%)/MCM-41. This indicates that some of the lattice oxygens( $O^{2-}$ ) in MCM-41 were replaced by oxygen vacancy( $O^-$ ) through mutual substitution of  $Pd^{2+}$  (86 pm),  $Ni^{2+}$  (135 pm), and  $Si^{4+}$  (110 pm) with different ionic radii. In addition, it has been suggested that the formation of Pd-s- $Si^{3+}$  may be found on the catalytic surface by electron transfer from Si to Pd due to electronegativity, where denotes an oxygen defect vacancy. The atomic percentage of Pd3d is 0.04.

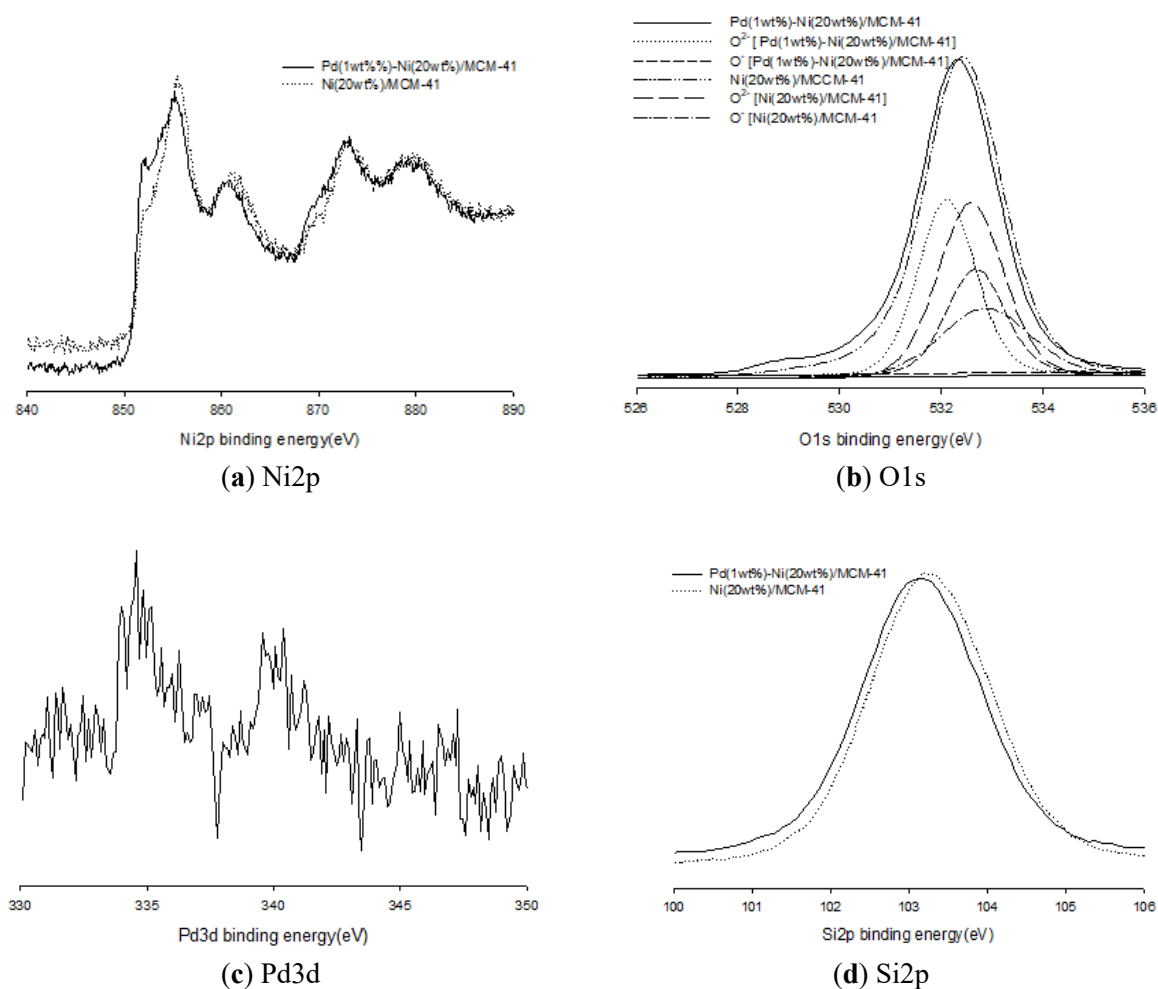
**Table 1.** Atomic percentage of core electron levels in fresh Pd(1wt%)-Ni(20wt%)/MCM-41 and Ni(20wt%)/MCM-41 based on XPS data.

Fresh Catalyst	Core Electron Levels	Atomic%
Pd(1wt%)-Ni(20wt%)/MCM-41	O1s	66.92
	Si2p	28.76
	Ni2p	4.27
	Pd3d	0.04
Ni(20wt%)/MCM-41	O1s	68.59
	Si2p	28.64
	Ni2p	2.77

This phenomenon is believed to enhance Ni2p dispersion owing to the appropriate metal-support interaction<sup>[8]</sup> by substituting some of  $Si^{4+}$  in  $SiO_2$  with  $Ni^{2+}$  or  $Pd^{2+}$  ions and oxygen vacancy formation — thereby maintaining the activity and stability and of Pd(1wt%)-Ni(20wt%)/MCM-41.

**Figure 3** shows the XPS spectra of (a) Ni2p, (b) O1s, (c) Pd3d, and (d) Si2p core electron levels for fresh Ni(20wt%)/MCM-41 and Pd(1wt%)-Ni(20wt%)/MCM-41 catalysts reduced before the reaction. The characteristic Ni2p<sub>3/2</sub> peaks for fresh Pd(1wt%)-Ni(20wt%)/MCM-41, namely  $Ni^0$ ,  $Ni^{2+}$ , and satellite, appeared at 850.28, 855.18, and 860.58 eV, respectively. Ni2p<sub>1/2</sub> peak, namely  $Ni^{2+}$  and satellite, appeared at 872.58 and 879.08 eV, respectively. For fresh Ni(20wt%)/MCM-41, the Ni2p<sub>3/2</sub> peaks, namely  $Ni^0$ ,  $Ni^{2+}$ , and satellite, appeared at 852.1, 855.31, and 860.88 eV, while the Ni2p<sub>1/2</sub> peaks, namely  $Ni^{2+}$  and satellite, appeared at 873.08 eV and 880.08 eV, respectively. The characteristic O1s peak for fresh Ni(20wt%)/MCM-41 appeared at 531.28 eV, while that for fresh Pd(1wt%)-Ni(20wt%)/MCM-41, corresponding to Si–O–Si binding energy exhibited a slight chemical shift toward lower energy than Ni(20wt%)/MCM-41. The  $O^{2-}$  and  $O^-$  peaks of fresh Ni(20wt%)/MCM-41 appeared at 532.58 and

532.86 eV, respectively. While those of fresh Pd(1wt%)-Ni(20wt%)/MCM-41 appeared at 532.11 and 532.68 eV, respectively, showing a slight chemical shift toward lower energy than Ni(20wt%)/MCM-41. Characteristic Pd3d<sub>5/2</sub> peak for fresh Pd(1 wt%)-Ni(20wt%)/MCM-41, namely  $Pd^0$ , appeared at 334.58 eV, while Pd3d<sub>3/2</sub> peak, namely  $Pd^0$ , appeared at 339.58 eV. Characteristic Si2p peak for fresh Pd(1wt%)-Ni(20wt%)/MCM-41, namely  $Si^{+4}$ , appeared at 103.21 eV, while fresh Ni(20wt%)/MCM-41 peak appeared at 103.72 eV. Compared to fresh Ni(20wt%)/MCM-41, the core electron levels such as Ni2p, O1s, and Si2p of fresh Pd(1wt%)-Ni(20wt%)/MCM-41 exhibited a slight chemical shift toward lower energy. Addition 1 wt% of Pd to the Ni(20wt%)/MCM-41 shifts binding energy of the core electrons level toward lower energy than Ni(20wt%)/MCM-41, probably owing to the charge transfer from Si to Pd and the change in the  $SiO_2$  lattice by NiPd alloy formation. In addition, the  $Pd^0$  is able to activate from  $CH_4$  to  $H_2$ , then decrease the binding energy by favouring the reduction of Ni ions by  $H_2$  spillover. Dogu et al.<sup>[6]</sup> reported that the addition of 0.5 wt% of Pd to Ni/MCM-41 improves the dispersion of Ni particles on the catalyst surface, and creates small nano-sized Ni particles, which easily reduce NiO particles.



**Figure 3.** XPS spectra showing (a) Ni2p, (b) O1s, (c) Pd3d, (d) Si2p core electron levels for fresh Pd (1wt%)-Ni (20wt%)/MCM-41 and fresh Ni (20wt%)/MCM-41.

These findings suggest that Ni ions in Pd(1wt%)-Ni(20wt%)/MCM-41 were more readily reduced owing to H<sub>2</sub> spillover compared to those in Ni(20wt%)/MCM-41, and the dispersion is enhanced on the catalyst surface owing to the appropriate metal-support interaction, where some Si<sup>4+</sup> in SiO<sub>2</sub> is substituted with Ni<sup>2+</sup> or Pd<sup>2+</sup> ions.

## 4. Conclusions

The H<sub>2</sub> production was achieved by performing CDM over PM(1wt%)-Ni(20wt%)/MCM-41 (PM = Pd, Pt, and Rh), Ni(20wt%)/MCM-41, and Pt(1wt%)/MCM-41 using a PBFR under atmospheric conditions. The addition of 1 wt% PM (Pd, Pt, and Rh) as a promoter to Ni(20wt%)/MCM significantly affected of CDM to H<sub>2</sub> yield. Pd(1wt%)-Ni(20wt%)/MCM-41 achieved approximately 1.5 times

higher H<sub>2</sub> yield than that of Ni(20wt%)/MCM-41. At  $1.2 \times 10^4$  s, the H<sub>2</sub> yield of catalysts in CDM followed the order of Pd(wt%1)-Ni(20wt%)/MCM-41  $\gg$  Pt(1wt%)-Ni(20wt%)/MCM-41 > Rh(1wt%)-Ni(20wt%)/MCM-41 > Ni(20wt%)/MCM-41  $\gg$  Pt(1wt%)/MCM-41. The NiPd crystallites formed through appropriate interaction between Ni<sup>2+</sup> and Pd<sup>2+</sup> ions promoted Ni2p enrichment on the MCM-41 surface, supporting the H<sub>2</sub> yield and stability of Pd(1wt%)-Ni(20wt%)/MCM-41. The Ni2p atomic percentage in Pd(1wt%)-Ni(20wt%)/MCM-41 also increased from 2.77% to 4.27% compared to that in Ni(20wt%)/MCM-41, while that of O1s decreased from 68.59% to 66.92%. The Ni2p, O1s, and Si2p core electron levels in fresh Pd(1wt%)-Ni(20wt%)/MCM-41 exhibited a slight chemical shift toward lower energy compared to those of Ni(20wt%)/MCM-41. Compared to Ni(20wt%)/MCM-41, the Pd(1wt%)-

Ni(20wt%)/MCM-41 is believed to increase Ni<sub>2</sub>p distribution owing to the appropriate metal-support interaction and earlier reduction from H<sub>2</sub> spillover, thereby maintaining the H<sub>2</sub> yield and the catalyst stability. The CDM is an environmentally friendly process that produces CO<sub>x</sub>-free H<sub>2</sub> rather than the POM and the SMR. In addition, economical green H<sub>2</sub> can be produced by using a catalyst of 1 wt% Pd onto Ni(20wt%)/MCM-41 in the CDM process.

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## Institutional Review Board Statement

Not applicable.

## Informed Consent Statement

Not applicable.

## Data Availability Statement

Data are contained within the article.

## Conflicts of Interest

The authors declare no conflict of interest, financial or otherwise.

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