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## ARTICLE

# As-Cast Microstructures of High Entropy Alloys Designed to Be TaC-Strengthened

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### ABSTRACT

In this work two new alloys were obtained by extrapolation from a well-known high entropy alloy, the equimolar CoNiFeMnCr one. This was done by the addition of carbon and of tantalum, Ta being one of the strongest MC-former elements. They were produced by conventional casting under inert atmosphere. The obtained microstructures were characterized by X-ray diffraction, metallography, electron microscopy, and energy dispersion spectrometry. Their hardness was also measured by hardness indentation. In parallel, the original CoNiFeMnCr alloy was also synthesized and characterized for comparison. The reference HEA alloy is single-phased with an austenitic structure, while the two {Ta, C}-added alloys are double-phased, with an austenitic matrix and interdendritic script-like TaC carbides. The matrixes of these HEA/TaC alloy are equivalent to an equimolar CoNiFeMnCr alloy to which 2 wt.% Ta is present in solid solution. The presence of the TaC carbides caused a significant increase in hardness which suggests that the HEA/TaC alloys may be mechanically stronger than the HEA reference alloy at high temperature.

## 1. Introduction

The past decade has seen the appearance of a new generation of alloys interesting for various uses needing high mechanical properties: the “high entropy alloy” principle (HEA). Since some of them can offer good general properties at high temperatures, they may compete with the superalloys which are used for a long time in the aeronautic industry (turbine disks and blades, for instance), power

generation (burners, hottest parts of turbines...) and industrial processes working at elevated temperature (tools for shaping molten glasses...) <sup>[1-3]</sup>. Many HEAs contain in equimolar quantities (or also in various quantities) and with different numbers of metals often belonging to the {Fe, Co, Ni, Cr, Mn} list <sup>[4,5]</sup>. These five elements constitute a quinary system, the thermodynamic description of which was studied until recently <sup>[6,7]</sup>. Beside the conventional foundry of equimolar FeCoNiCrMn alloys, different

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ways of elaboration of superalloys were recently applied to HEAs: single crystalline growth<sup>[8]</sup>, additive manufacturing<sup>[9]</sup> or thin film deposition<sup>[10]</sup>. Their behaviors in case of extreme conditions of solicitations were also explored, mechanical properties<sup>[11,12]</sup> or chemical reactivity at high temperature<sup>[13]</sup>. Evolutions of chemical composition - variation of the Co or Ni content<sup>[14]</sup> (and even suppression of Co<sup>[15]</sup> or of Ni<sup>[16]</sup>) - were tested, and the notion of “Medium Entropy Alloys” has also appeared<sup>[17]</sup>. Nanoparticles of SiC particles have also started to be introduced in HEAs<sup>[18]</sup>.

The equimolar FeCoNiCrMn alloys are not far from cobalt-based superalloys, strengthened by solid solution, or from the matrix of polycrystalline cobalt-based superalloys with grain boundaries strengthened by carbides. Indeed, these cobalt-based superalloys are generally rich in nickel and in chromium, at least. The contents are not equivalent (50 wt.% Co or a little more, 10 wt.% Ni and 30 wt.% Cr) but one can guess that HEAs involving these elements may usefully contain primary chromium carbides or MC carbides as additional phases. The additional presence of such second phase (and third phase in some cases) is likely to push upwards the mechanical resistance at high temperature of HEAs, the matrix intrinsic strength of which can become no longer sufficient. A particular beneficial effect can be expected from the use of TaC carbides earlier successfully tested in polycrystalline chromium-forming cobalt-based model or industrial alloys<sup>[19,20]</sup>.

The aim of this work is to start investigating the principle of {*in situ* precipitated}-interdendritic script-like MC carbides, by synthesizing several HEA-based alloys in which the formation of MC carbides is promoted by the addition of carbon and of Ta, in quantities having earlier led to MC populations in adequate fractions<sup>[19,20]</sup>. Checking the reproduction of alloys similar to the model alloys cited above but with a matrix equivalent to a HEA, and characterizing their as-cast microstructures as well as their room temperature hardness, are the objectives of this work.

## 2. Materials and Methods

The three alloys were prepared by mixing pure elements: Co (centimetric flakes), Ni (millimetric balls), Fe (centimetric flakes), Mn (centimetric flakes) and Cr (centimetric blocks) for the “HEA” alloy, with additionally C (millimetric graphite rods) and Ta (millimetric slugs). The purity of all elements was > 99.9 wt.% (Alfa Aesar and Aldrich). The charges were weighed with accuracy to reach 40 g and the following contents:

- Equimolar CoNiFeCrMn, alloy called “HEA ref.”;
- 96 wt.% (CoNiFeCrMn) - 0.25 wt.% C - 3.72 wt.% Ta,

alloy called “HEA/TaC1”;

- 92 wt.% (CoNiFeCrMn) - 0.50 wt.% C - 7.44 wt.% Ta, alloy called “HEA/TaC2”.

Each mix of elements was placed in a copper crucible equipping a high frequency induction furnace (CELES, France; power: 50 kW). This metallic crucible was continuously cooled by circulating water at ambient temperature during the elaboration steps.

After introduction of the mix of pure elements, a silica tube was placed around the crucible and closed to allow the evacuation of the present air, operated by pumping. Crucible and silica tube were surrounded by a water-cooled copper coil in which an alternative current circulated. The frequency of the alternative current was between 100 kHz and 150 kHz, and the applied voltage was between 4 kV and 5 kV, this depending on the alloy. After 3 cycles made of pumping until  $4 \times 10^{-5}$  bars followed by filling by pure Argon, the internal atmosphere was considered as being pure Ar, with a pressure rated at about 400 mbars.

Heating led to the melting of the charges made of pure elements, and the obtained liquid alloy was maintained at the highest reached temperature during fifteen minutes to achieve total melting and chemical homogeneity for the liquid. During the cooling, produced by decreasing the input power/voltage, the alloys started solidifying, and later cooled in solid state. After about 20 minutes to 30 minutes, the obtained ingots were again at room temperature and they were extracted from the crucible.

Each ingot was first embedded in a cold resin mixture (ESCIL, France) to be more easily cut using a metallographic saw to produce a sample with the adequate shape and size to prepare a metallographic sample. The cut part was embedded in the cold {resin + hardener} mixture. The obtained embedded alloy samples were ground by using first #600-grade SiC papers, and second #1200-grade papers. Final polishing was carried out using a textile disk enriched with 1  $\mu$ m hard particles.

The obtained mirror-like samples were put, one after one, in the chamber of a Scanning Electron Microscope/SEM, model JSM-6010LA (JEOL, Japan). Their microstructures were observed in Back Scattered Electrons mode/BSE (acceleration voltage: 15 kV), at different magnifications. The Image J software was used to measure the surface fractions of the present particles (on three  $\times$  1000 SEM/BSE images per alloy). Energy Dispersive Spectrometry was used to control the obtained chemical compositions by full frame analysis (at the  $\times$  250 magnification). Additionally, spot analyses were performed on the visible particles to identify them and to specify the chemical composition of the matrix. X-ray diffraction/XRD was

also carried out for all alloys to complete the identification of the present phases. This was done using a D8 Advance diffractometer from Bruker (wavelength of the  $K\alpha$  transition of Cu).

The metallographic samples were also subjected to indentation tests to assess the hardness of all alloys. This was carried out using an automatic indentation machine (PRESI, France), according to the Vickers method. The applied load was 10 kg for all tests. Five indentations were carried out per alloy.

### 3. Results

#### 3.1 Microstructure and Composition of the “HEA ref.” Alloy

X-ray diffraction (XRD) carried out on the reference alloy designed to be CoNiFeMnCr equimolar led to the diffractogram given in Figure 1. This one demonstrates that the alloy is single-phased and contains only a Face Centered Cubic solid solution. This is confirmed by the observation of the microstructure of the metallographic sample using the SEM in BSE mode, illustrated by the SEM/BSE micrograph provided in Figure 2 together with an EDS spectrum showing the peaks of the elements

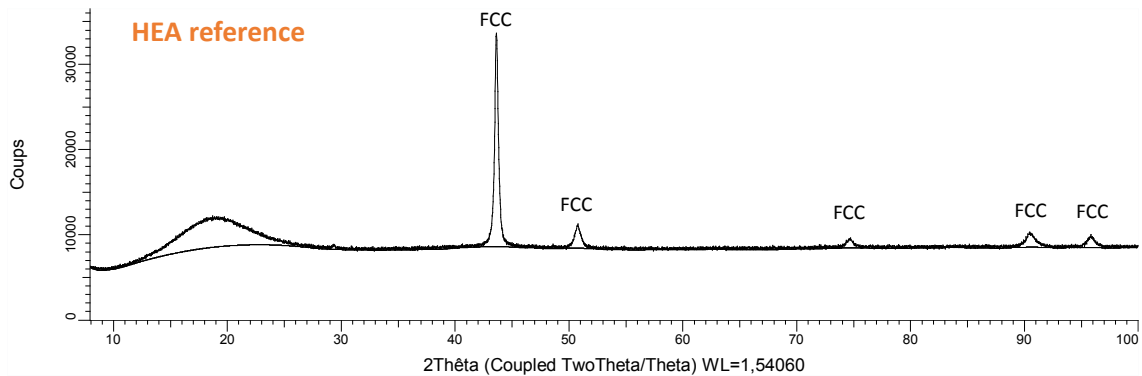
present in the alloy. The alloy effectively appears as single-phased while the EDS results (Table 1 and Table 2) confirm that the alloy is really equimolar.

**Table 1.** Chemical composition in weight percent of the reference alloy (average and standard deviation calculated from the results of three  $\times$  250 full frame areas)

HEA ref. Whole alloy	Wt.% Co	Wt.% Ni	Wt.% Fe	Wt.% Mn	Wt.% Cr	
Average content	19.8	21.4	19.5	19.5	19.8	
Standard deviation	0.2	0.2	0.1	0.0	0.1	

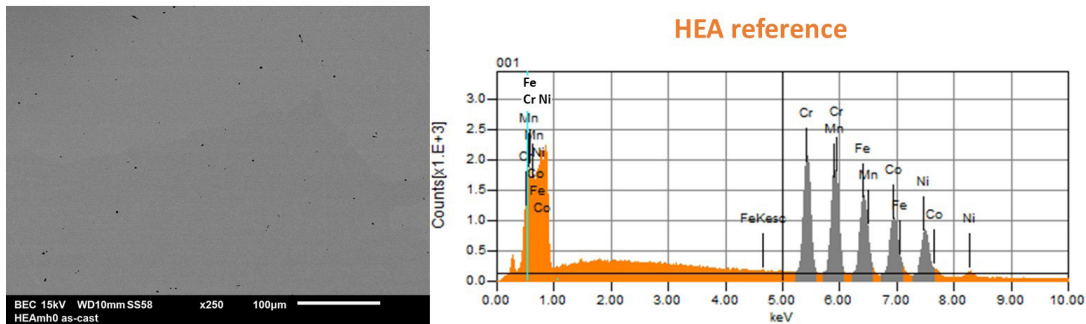
**Table 2.** Chemical composition in atomic percent of the reference alloy (average and standard deviation calculated from the results of three  $\times$  250 full frame areas)

HEA ref. Whole alloy	At.% Co	At.% Ni	At.% Fe	At.% Mn	At.% Cr	
Average content	18.9	20.4	19.5	19.9	21.3	
Standard deviation	0.1	0.2	0.1	0.0	0.1	



**Figure 1.** Diffractogram of the HEA reference alloy

(peaks indexed by “FCC”: Face Centered Cubic crystalline network of the single phase)



**Figure 2.** SEM/BSE micrograph of the microstructure of the HEA reference alloy (left) and EDS spectrum acquired on this area (right)

An elemental map was also acquired on the HEA reference alloy to study its chemical homogeneity (Figure 3). It allows observing that all elements are rather homogeneously distributed in the single phase, except manganese which is more present in areas looking as interdendritic spaces.

### 3.2 Microstructures and Compositions of the {Ta,C}-Containing Alloys

The X-ray diffractograms are acquired on the two alloys resulting from the addition of tantalum and carbon (Figure 4) both contain all the peaks corresponding to the FCC solid solution CoNiFeMnCr already featuring in the diffractogram of the HEA reference alloy (Figure 1). Additional peaks are also present: they correspond to the TaC phase. The microstructures of these two {Ta, C}-containing alloys are illustrated by SEM/BSE micrographs in Figure 5 together with the EDS spectra acquired on these zones. The global chemical compositions of these two alloys measured by full frame EDS analysis on three distinct zones (magnification  $\times 250$ ) and the chemical composition of the matrix measured by spot analysis in three distinct locations, are given in Table 3 for the HEA/TaC1 alloy and in Table 4 for the HEA/TaC2 alloy. Obviously the two alloys each contain at least two phases, including a dendritic matrix. The global chemical compositions are globally well respected.

The microstructure of the HEA/TaC1 alloy is composed of a dendritic matrix and of an interdendritic compound. Observations at higher magnification (Figure 6, left) allow distinguishing two phases in the interdendritic compound. This compound is made of a part of matrix (identified by EDS spot analysis) and of white particles. These ones are TaC carbides, the presence of which was already shown by XRD. The TaC composition was evidenced by spot EDS analysis performed on the coarsest white particles found: almost exclusive presence of Ta and C, and molar equivalence between Ta and C. Due to its interdendritic location and to its constitution in two phases closely imbricated, this compound is certainly of a eutectic nature; it precipitated at the end of solidification with the simultaneous growth of additional matrix and TaC carbides.

Although similar to the HEA/TaC1 one (presence of a dendritic matrix, {matrix + TaC} compound), the microstructure of the HEA/TaC2 alloy presents a particularity since it also contains in addition blocky white particles. EDS spot analysis shows that there are also TaC carbides.

The surface fractions of the TaC phase were measured on three randomly chosen  $\times 1000$  SEM/BSE micrographs for the two alloys, using the Image J software, after having rated the threshold to isolate the white TaC from the gray matrix. The HEA/TaC1 alloy contains about 6.4 surf.% of TaC and the HEA/TaC2 contains 11.2 surf.% TaC (average values).

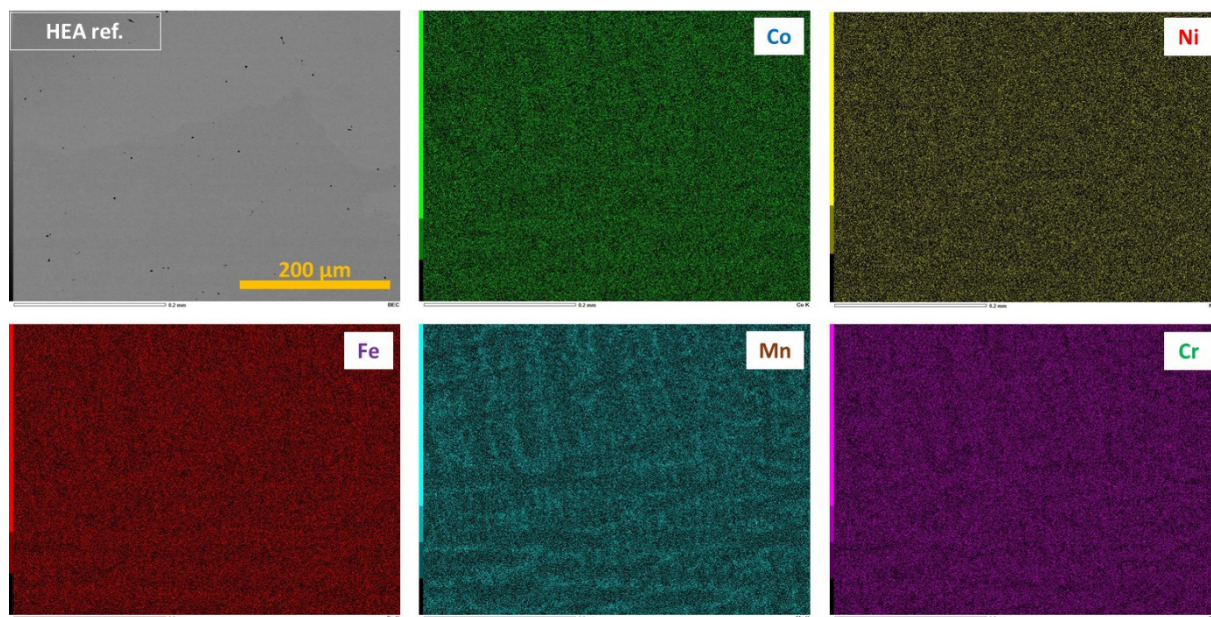
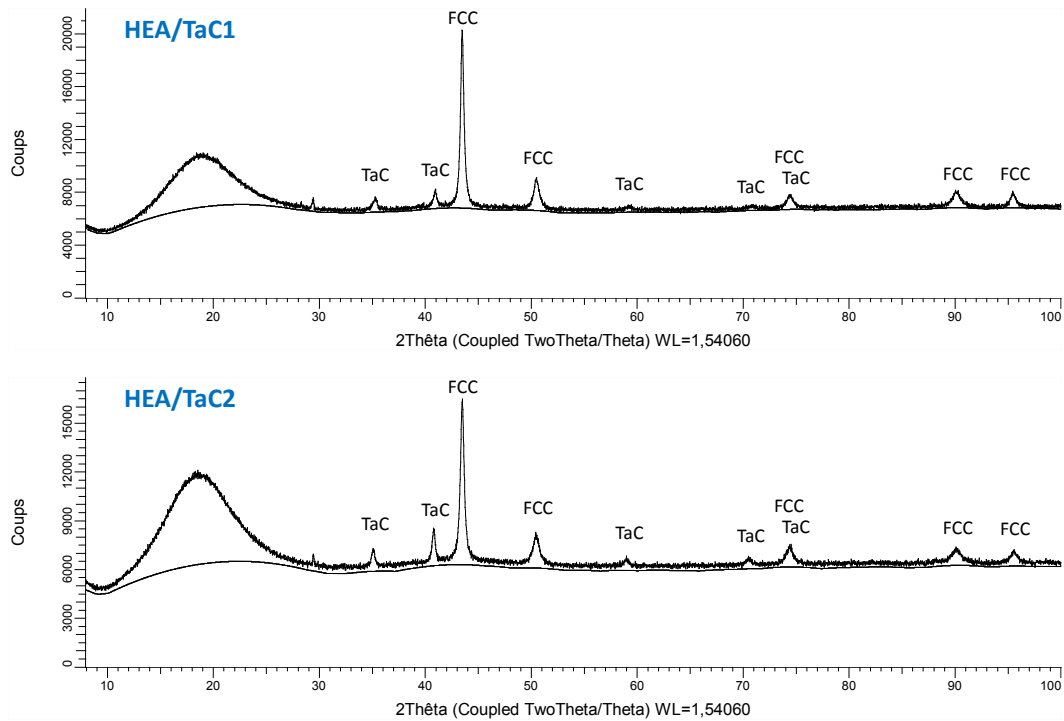
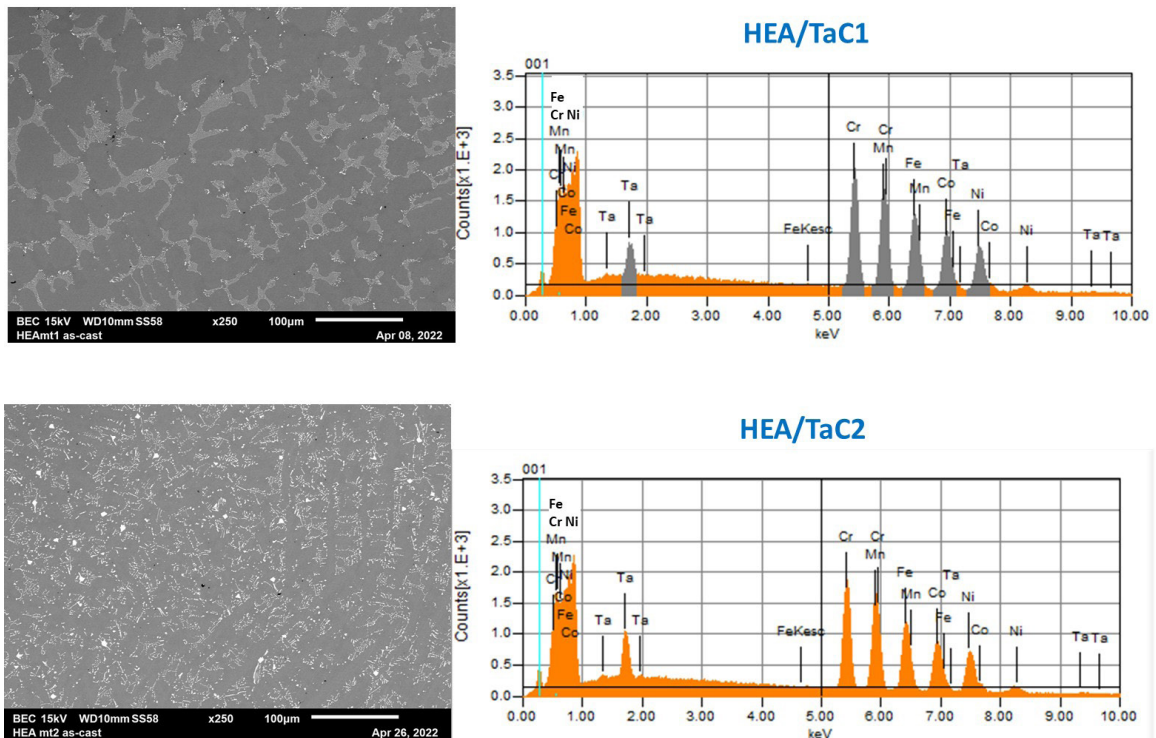


Figure 3. X-maps obtained on the HEA reference



**Figure 4.** Diffractograms of the HEA/TaC1 (top) and HEA/TaC2 (bottom) alloys



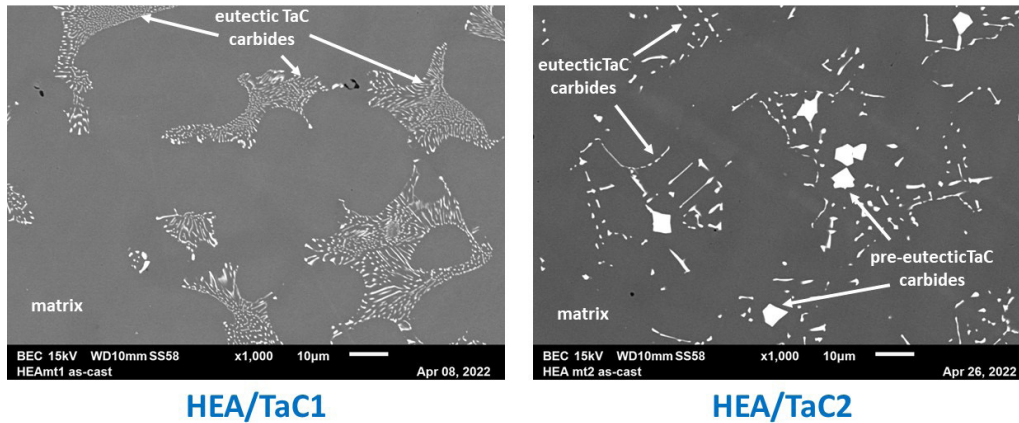
**Figure 5.** SEM/BSE micrographs of the microstructure of the HEA/TaC1 alloy (top, left) and EDS spectrum acquired on this area (top, right), and of the HEA/TaC2 alloy (bottom left) and the corresponding EDS spectrum (bottom, right)

**Table 3.** General chemical compositions of the HEA/TaC1 alloy (average and standard deviation calculated from the results of three  $\times$  250 full frame areas) and chemical compositions of its matrix (all contents in weight percent, carbon not possible to analyze but supposed to be well respected: 0.25 wt.% C)

HEA/TaC1 Whole alloy	Wt.% Co	Wt.% Ni	Wt.% Fe	Wt.% Mn	Wt.% Cr	Wt.%Ta
Average content	19.3	20.1	18.6	18.3	19.2	4.5
Standard deviation	0.2	0.5	0.5	0.3	0.3	0.4
HEA/TaC1 Matrix	Wt.% Co	Wt.% Ni	Wt.% Fe	Wt.% Mn	Wt.% Cr	Wt.%Ta
Average content	20.5	20.5	20.9	16.7	19.4	2.1
Standard deviation	0.4	0.3	0.9	1.4	0.6	0.1

**Table 4.** General chemical compositions of the HEA/TaC2 alloy (average and standard deviation calculated from the results of three  $\times$  250 full frame areas) and chemical compositions of its matrix (all contents in weight percent, carbon not possible to analyze but supposed to be well respected: 0.5 wt.% C)

HEA/TaC2 Whole alloy	Wt.% Co	Wt.% Ni	Wt.% Fe	Wt.% Mn	Wt.% Cr	Wt.TaC
Average content	18.5	20.0	17.9	18.1	19.1	6.3
Standard deviation	0.5	0.2	0.5	0.2	0.3	0.7
HEA/TaC2 Matrix	Wt.% Co	Wt.% Ni	Wt.% Fe	Wt.% Mn	Wt.% Cr	Wt.%TaC
Average content	18.2	22.8	16.2	22.1	18.9	1.9
Standard deviation	0.5	1.2	2.1	2.0	0.3	0.4



**Figure 6.** High magnification SEM/BSE micrographs for observation in details of the microstructures of the two {Ta, C}-containing HEA alloys (left: HEA/TaC1, right: HEA/TaC2)

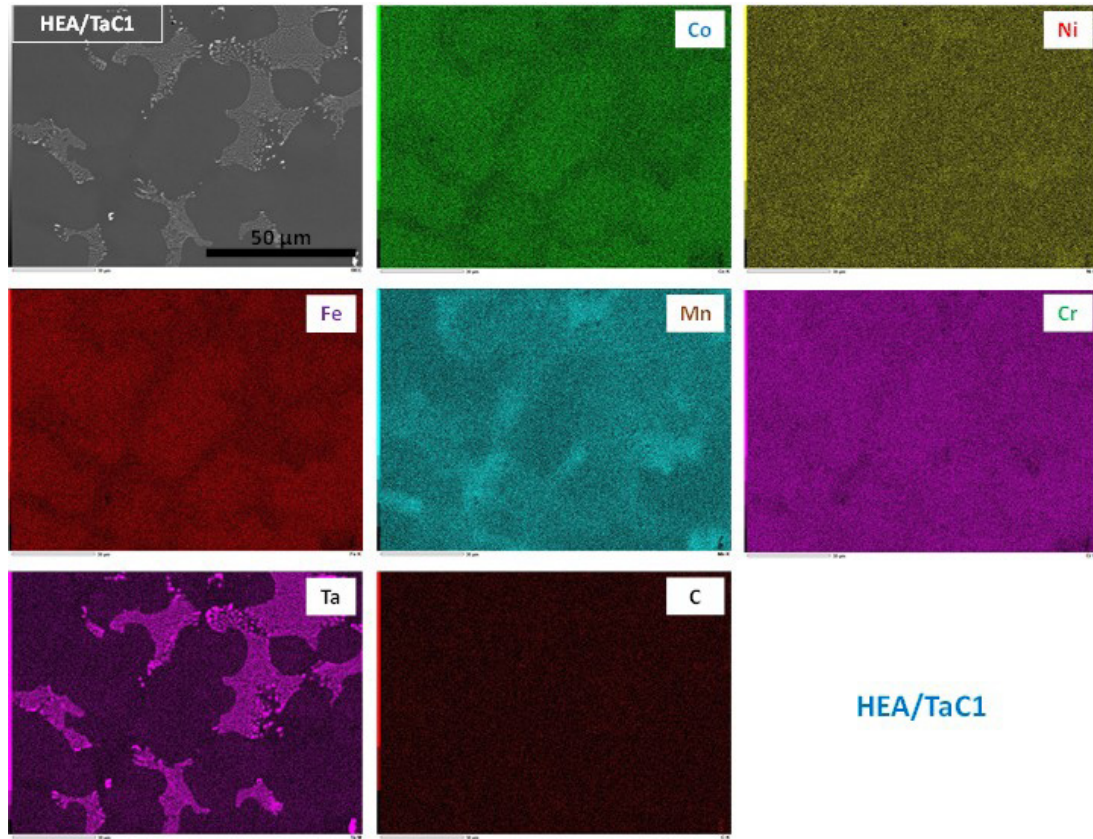
Several EDS spot analyses were also carried out in the matrixes of both alloys (bottom parts of Table 3 and Table 4). Unsurprisingly (since there is only a second phase which is TaC carbide in both alloys), the matrixes are equimolar in Co, Ni Fe, Mn and Cr. But they also contain about 2 wt.% Ta, showing that only a part of tantalum is involved in carbides. A part of carbon is consequently also necessarily present in solid solution in the matrix but, unfortunately, it cannot be analyzed.

One can also notice that the Mn and Fe contents seem varying in the matrix of each alloy. The X-maps presented in Figure 7 effectively evidences in the case of the HEA/

TaC1 alloy, slight but real variations in Mn content in its matrix. One encounters again what was observed in the HEA ref. alloy in Figure 3.

### 3.3 Hardness of the HEA ref. and HEA/TaC Alloys

Per alloy, five indentations were carried out according to the Vickers method, with a 10 kg load. The results, displayed in Table 5, are available for comparison with the hardness of the HEA reference alloy. It clearly appears that the presence of carbides induced a significant increase in hardness.



**Figure 7.** X-maps obtained on the HEA/TaC1 alloy

**Table 5.** Hardness of the HEA/TaC alloys in comparison with the HEA reference alloy

Vickers 10 kg 5 indent.	HEA ref.	HEA/TaC1	HEA/TaC2
Average content	121	180	194
Standard deviation	2	4	5

## 4. Discussion

The first alloy to be produced with the apparatus used here (High Frequency Induction furnace, fusion and solidification achieved in a unique water-cooled copper crucible) and the elaboration protocol (all the operating parameters applied here) was the HEA ref. one. It was successfully obtained as a single-phased austenitic alloy, as it is obtained by all researchers working on this type of HEA alloy. The elemental distribution was globally homogeneous, except concerning Mn. The two HEA/TaC alloys themselves presented a matrix globally homogeneous, except Mn again. In their case, the presence of interdendritic particles allowed evidencing that the Mn-enriched zones of the matrix were close to the interdendritic spaces, and thus that Mn was subjected to positive segregation. The knowledge of this not perfect chemical homogeneity of the matrix allows thinking to apply a homogenization heat treatment prior to the use of these alloys, since this small lack of homogeneity can be deleterious for some properties.

The addition of Ta and of C successfully led to an interesting population of carbides. TaC formed at the expense of other types of carbides, notably at the expense of chromium carbides as this previously occurred in earlier alloys fabricated following the same elaboration way and similar protocols (in Ni-30Cr-0.2 or 0.4C-3 or 6Ta<sup>[21]</sup>). In that way, the 20 wt.% Ni in presence of 20 wt.%Cr is probably compensated by the 20 wt.% Co and 20 wt.% Fe more favorable to the formation of TaC. Indeed, these two last elements did not cause earlier problem of predominance of chromium carbides on TaC carbides in Cr-rich alloys for which they were the base elements<sup>[22-24]</sup>.

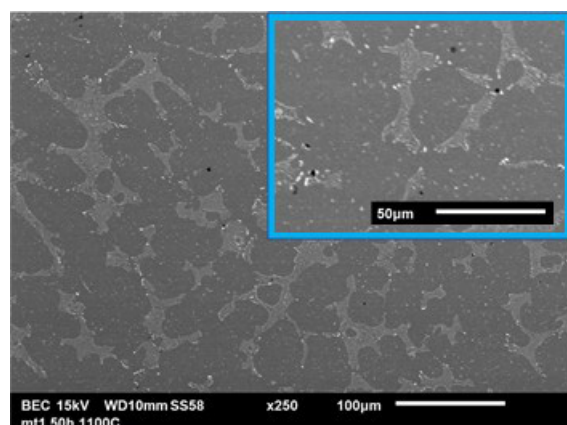
As in the earlier studied Cr-rich alloys based on Co<sup>[22]</sup> or on Fe<sup>[23,24]</sup>, the TaC carbides obtained here have appeared in the last zones to solidify and they are essentially eutectic with close imbrication with matrix, and of the script-like morphology. Good initial interdendrites and intergrains cohesion at high temperature can be thus expected on long time for delaying the transition from secondary state of creep to the tertiary state. It is true that other TaC particles - coarse blocky carbides not mixed with matrix - are present in the HEA/TaC2 alloy, but one can think that they can be not detrimental for the mechanical properties at high temperatures. These blocky TaC are similar to the ones previously observed in cobalt-chromium alloys with high contents in Ta en C (15 wt.% and 1 wt.% C) earlier studied<sup>[25]</sup>. In these alloys earlier studied, thermodynamic calculations evidence that low C and Ta contents led to the appearance of eutectic TaC carbides only, the dendritic matrix being thus the first solid phase to crys-

tallize from the liquid state. In contrast, higher C and Ta contents induced the pre-eutectic crystallization of a first TaC population instead of the matrix. These pre-eutectic TaC carbides grew, freely in the liquid, with a blocky and angular shape and became the coarse carbides not necessarily located in the interdendritic spaces observed in the metallographic samples. The origin of the blocky carbides observed in the HEA/TaC2 alloy is certainly the same: moving from {0.25 wt.% C, 3.7 wt.% Ta} to {0.50 wt.% C, 7.4 wt.% Ta} obviously induced here too change of location of the alloy from one side of the eutectic valley to the other side, with as consequence a solidification of first TaC and second TaC & matrix, instead a solidification of first matrix and second TaC & matrix. By comparison with these earlier studied cobalt-based alloys, the replacement of a great part of cobalt by new elements to achieve equal proportions in Co, Ni, Fe, Cr and Mn, has obviously caused a displacement of the eutectic valley toward lower tantalum and carbon contents.

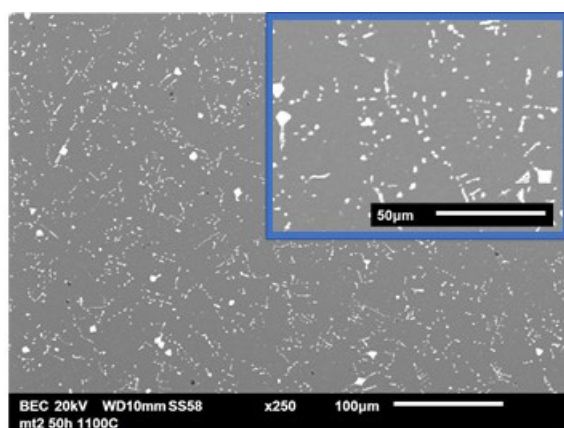
To speak again about the matrix, this one is not really an equimolar alloy since it contains also 2 wt.% Ta. This is the typical Ta content in the matrix of Cr-rich Co-based alloys containing 0.2C-3Ta or 0.4C-6Ta (wt.%)<sup>[22]</sup> (and twice the one in the Cr-rich Fe-based alloys with the same C and Ta contents<sup>[23]</sup>, or half the one in the Cr-rich Fe-based alloys with the same C and Ta contents<sup>[21]</sup>). The presence of Ta in solid solution in the matrix did not change its single-phase state and it may possibly bring an additional strengthening.

Concerning the properties of these TaC-strengthened alloys at high temperature, an ongoing study has brought first results of microstructure behavior. They are illustrated in Figure 8. After 50 h at 1100 °C, no start of local melting was detected. Furthermore, the TaC carbides population has not significantly changed. The script-like shape of the eutectic carbides is kept, despite a limited fragmentation and the pre-eutectic blocky carbides of the HEA/TaC2 alloy are not affected. There is another modification which is interesting to notice: the precipitation of fine carbides from the Ta and C initially present in solid solution in the matrixes of the as-cast alloys. This is a potential source of additional strengthening which can be useful during the steady state of creep deformation (secondary step of creep). These secondary TaC are more numerous in the HEA/TaC1 alloy than in the HEA/TaC2 alloy. In this second alloy, the higher density of primary TaC led Ta and C diffusing towards the neighbor carbides to precipitate on their surfaces. The contribution of fine dispersed TaC carbides will be thus more useful for the HEA/TaC1 alloy than for the other alloy. Creep tests are scheduled on these HEA/TaC1 and HEA/TaC2 alloys to assess the progress

in strength at high temperature due to these TaC carbides added to the HEA reference alloy.



HEA/TaC1 after 50h at 1100°C



HEA/TaC2 after 50h at 1100°C

**Figure 8.** Microstructures of the two HEA/TaC1 (left) and HEA/TaC2 (right) alloys after 50 hours at 1100 °C (SEM/BSE at the  $\times 250$  magnification and at  $\times 500$  in the top right corners).

## 5. Conclusions

The as-cast microstructures obtained for the new alloys resulting from the addition of Ta and C to an equimolar CoNiFeMnCr HEA alloy are thus composed of a matrix similar to a HEA alloy, despite the presence of Ta (and C) in solid solution in proportion much lower than the first five elements, and of interdendritic TaC carbides forming a eutectic compound with the peripheral parts of the matrix dendrites. The combination of these two phases can be potentially very interesting, knowing the good properties of equimolar CoNiFeMnCr alloys (furthermore possibly enhanced by Ta in solid solution) and the script-like TaC carbides which have earlier demonstrated their beneficial effect for the creep resistance of Cr-rich Co-based superalloys. Now, the morphological sustainability of the script-

like TaC carbides on long term at high temperature needs to be tested, and the mechanical properties are to be tested in hot conditions, by creep tests for instance. Another important point to check is the behavior of these HEA/TaC alloys in oxidation at high temperature. This one risks to be not sufficient because of the rather low chromium content to which the equimolar criterion led. These investigations of the microstructure, mechanical and oxidation properties at high temperature are being done in new ongoing studies.

## Author Contributions

This present study is the own work of the single author.

## Conflict of Interest

There is no conflict of interest for this work.

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ARTICLE

# Spatial Investigation of Nilüfer Stream Arsenic Pollution in Previous and Post COVID-19 Pandemic and Evaluation of Health Risks for Adult People

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ABSTRACT

This study was carried out in Nilüfer Stream in Bursa City, where intensive industrial, agricultural and mining activities are existed. The temporal and spatial variation of arsenic was evaluated by examining its concentrations between March 2015 and December 2021. Values between March 2015 and December 2019 were evaluated as pre-pandemic, and values between March 2020 and December 2021 were evaluated as post-pandemic. The results were compared with national and international standards and the chronic and cancer risks were calculated for adults. When the 7-year general averages were examined, it was seen that the highest concentration was 0.0256 mg/L at the 8th Station, and the lowest concentration was 0.0182 mg/L at the 1st Station. The reason why the highest value is at the 8th station was that the wastewater of Nilüfer and Bursa Organized Industrial Zones was discharged to Bursa West Wastewater Treatment Plant before this station. After the pandemic the raises in concentrations were observed at all stations, except for the 3rd Station. This shows that the pollution load had increased in general during the pandemic. However, it was estimated that there was a decrease in the pollution load of the industrial wastewater coming to the 3rd Station, which was located after the Eastern Wastewater Treatment Plant of the City. It was observed that all stations examined were higher than drinking water standards and lower than irrigation water standards according to WHO and Turkish National Standards. All measuring stations were greater than 1 of the hazard quotient (HQ) values. In terms of human consumption risk, all stations had a chronic and carcinogenic risk according to the values before and after the pandemic. After the pandemic conditions, the HQ order of the stations was  $8 > 10 > 7 > 9 > 2 > 6 > 4 > 1 > 3$ . In general, post-pandemic HQ values had generally increased and the risk of cancer had increased.

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## 1. Introduction

Arsenic occurs naturally in the earth's crust and is an element classified as a semi-metal or metalloid. Arsenic could enter waters from pesticides and phosphate fertilizers, mine drainage, oxidation of arsenic-containing sulfide minerals, reduction of arsenic-bearing iron and manganese oxides, discharges of geothermal waters and power plants, improper production, use and disposal of arsenic-containing products<sup>[1,2]</sup>. Industrial productions containing arsenic include wood, timber preservation, cosmetics, paint enterprises, pharmaceutical industry, herbicide industry, semiconductor material production, leather, glass production, medical uses, paper and pulp production, and cement enterprises. In addition, copper, nickel, gold mining and ore disposal operations, agricultural practices, use of fossil fuels, landfill leachate are among the anthropogenic sources of arsenic<sup>[3,4]</sup>.

In the report titled "Human Development Report 2006 on the Verge of Scarcity: Power, Poverty and the Global Water Crisis" prepared by the United Nations Development Program, Turkey had been shown among the countries with the possibility of arsenic contamination<sup>[3]</sup>. High levels of arsenic had also been detected in Bursa and its environs, as well as in Balıkesir and Uşak<sup>[5,6]</sup>. The Nilüfer Stream, which passes through Bursa, where the textile, automotive, metal and chemical industries were intense, agricultural production and mining was carried out, and which was the 4th largest city of Turkey, is under intense pressure in terms of metal pollution<sup>[7-9]</sup>. There was Emet and Orhaneli Stream within the borders of Bursa City. In the Uluabat Lake Basin formed by the Emet and Orhaneli Streams, there were Keles Lignites Enterprise, Tunçbilek Coal Enterprise, Tunçbilek Thermal Power Plant and Emet Colemanite enterprises on the Emet Stream. It was stated in the literature that the colemanites of the region contain arsenic in the form of orpiment and realgar<sup>[10]</sup>. It was known that mineralized coal types were rich in toxic trace elements such as arsenic, mercury, antimony, and thallium. Arsenic was mixed into the waters in Uluabat Lake and its Basin, where mining was carried out intensively<sup>[10]</sup>. The 5 wastewater treatment plants located in the Nilüfer Stream Basin discharged the treated industrial and domestic wastewater to the Stream<sup>[8]</sup>. It was thought that the use of herbicides containing arsenic compounds in Bursa, which was an important agricultural center in Turkey, causes soil and water pollution<sup>[11]</sup>.

Within the scope of this study, the variation of As pollution between the years 2015-2021 at the measurement stations on the side and main branches of the Nilüfer Stream was investigated. Also, it was aimed to observe the effects of the COVID-19 pandemic on As pollution and to

examine the concentration trends in the last 7 years. This study was scientifically original because it was shown the effect of the COVID-19 pandemic on As pollution.

## 2. Materials and Methods

### 2.1 Study Area

Nilüfer stream which arises from the border of Bursa city served as an important water supply for the city and reaches the sea after a long flow in the basin. The Nilüfer stream had been exploited to support agriculture and the public water supply. The major sources of pollutants of Nilüfer stream come from point sources which were mainly composed of treated wastewater discharges from organized industrial districts and municipal sewage treatment plants. There were 5 large wastewater treatment plants in the Nilüfer Stream Basin. Two of them (Demirtaş and Bursa Organized Industrial Zones Wastewater Treatment Plant) had a completely industrial wastewater characterization, while the Eastern, Western and Green Environment Wastewater Treatment Plants had domestic and industrial characterization. Also, non-point sources were mainly composed of surface run-off from agricultural areas<sup>[7]</sup>.

In Bursa City, apart from textile, automotive, metal, and chemical industry, wastes arising from the processing of many marble quarries, tungsten, lignite, boron, magnesite, zinc, asbestos, chromium, and olivine ores were found in the basin. In addition, there was 1 coal-fired thermal power plant in the province<sup>[12]</sup>.

Samples were taken from 10 different points, upstream and downstream of the Nilüfer Stream, before and after the wastewater treatment plants. The locations of the measuring stations were given in Table 1 and Figure 1.

**Table 1.** Locations of the measuring stations

Station No	Location
1	On Nilüfer Stream, Gümüştepe Locality
2	On Deliçay Creek, Before Discharge of East wastewater treatment plant
3	On Deliçay Creek, After Discharge of East wastewater treatment plant
4	On Nilüfer Stream, After Deliçay Creek Mixture
5	İsmetiye Stream
6	On Nilüfer Stream, After Dosab Wastewater Treatment Plant Discharged
7	On Ayvalı Creek Before West Wastewater Treatment Plant Discharge
8	On Ayvalı Creek, After West Wastewater Treatment Plant Discharge
9	On Hasanağa Creek
10	On Nilüfer Stream, After Hasanağa Creek Mixture

## 2.2 Laboratory Analyses

Water samples were collected from midstream at a depth of 15 cm ~ 20 cm in 1000 mL polyethylene bottles, which had previously been cleaned by soaking in 10% nitric acid and rinsed with distilled water. At the sampling site, the bottles were rinsed twice with the water to be sampled prior to filling. The water samples were acidified on site to a pH less than 2 with 5 mL of analytical grade concentrated  $\text{HNO}_3$ . After collection the samples were placed in coolers with ice bags while being transported to the laboratory and kept at about 4 °C until being analyzed<sup>[8,13]</sup>. Grab samples were collected in dry weather conditions from the 10 measuring stations seasonally (March, June, September, and December) between 2015 and 2021.

Water samples were implemented digesting process via a CEM MARS-5 model microwave instrument. A 40 mL sample was placed into the cell and then 6 mL of  $\text{HNO}_3$  (65% analytical grade) and 4 mL of HCl (37% analytical

grade) were added to the cell. 180 psi pressure and 160 °C temperature was applied for 20 minutes to the cell. After cooling 30 minutes to room temperature samples transferred into a 100 mL flask. The digested samples were filled with distilled water to the 100 mL mark, and used in the ICP-AES (Vista MPX, Varian) analysis. The standard calibration solutions were prepared at concentrations of 0.05 mg/L, 0.1 mg/L, 0.25 mg/L, 0.5 mg/L, and 1 mg/L. For higher than 1 mg/L of samples, calibration solution concentrations were prepared at 1 mg/L, 2 mg/L, 5 mg/L, and 10 mg/L. The blanks were done by concentrated 5%  $\text{HNO}_3$  into ultrapure water. Quality control was performed with certified liquid samples (multi-elements standard, catalogue number 900-Q30-002, lot number SC0019251, SCP Science, Lasalle, Quebec) to provide the accuracy of the measurements. Quantification limit was 5 µg/L for As. Certified liquid samples were used to check the analytical accuracy, which ranged between 1% and 10%. All reagents used were of analytical grade or better<sup>[13]</sup>.

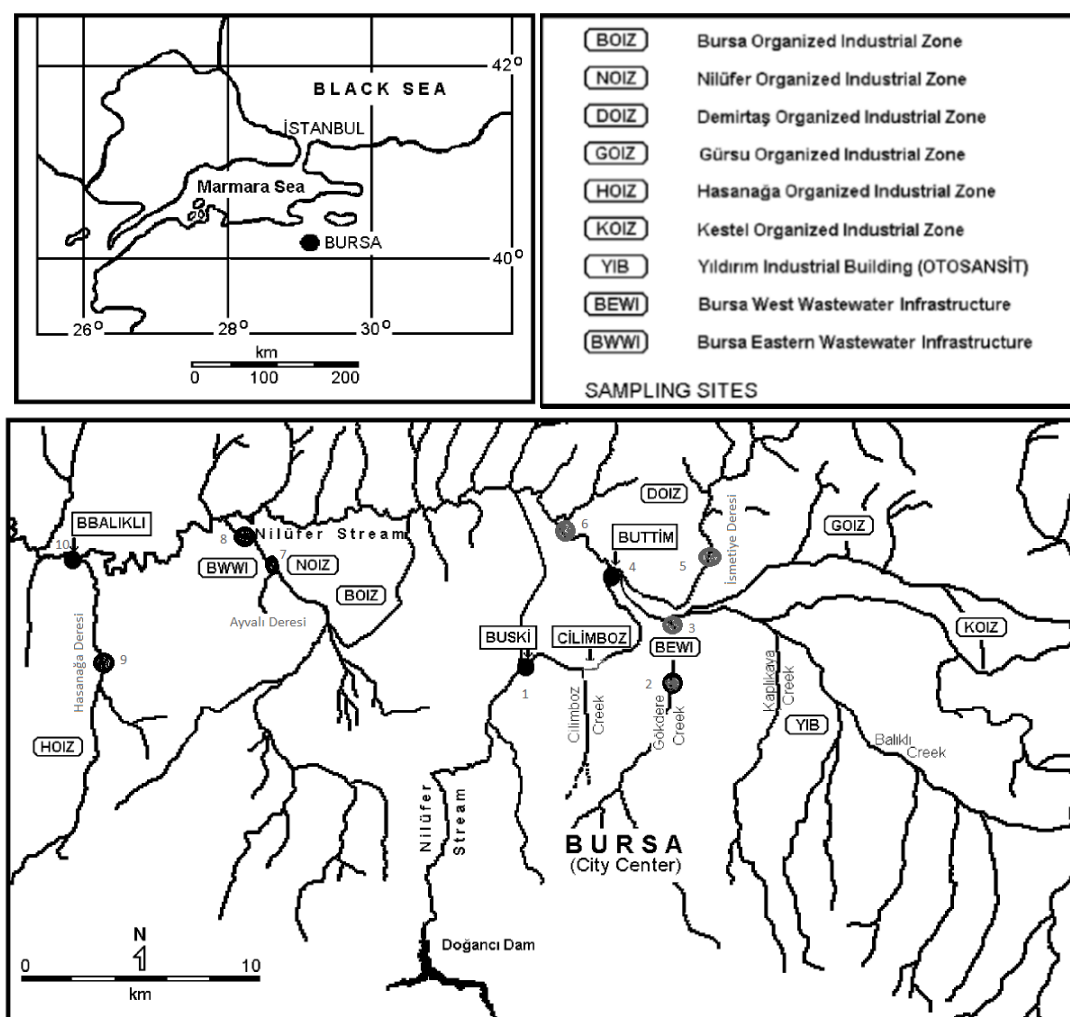


Figure 1. Location of Measuring Stations (Adapted from Güleriyüz et al., 2008)<sup>[14]</sup>.

## 2.3 Evaluation of the Health Risk of Arsenic

Arsenic enters into human body by the way of nutrition, dermal contact and inhalation<sup>[15]</sup>. The average daily dose (ADD) through potable water intake was estimated according to the following equation<sup>[16,17]</sup>.

$$ADD = C \times IR \times ED \times EF / (BW \times AT) \quad (1)$$

In this equation ADD was the average daily dose during the exposure (mg/kg-day) and C represented the arsenic concentration in water (µg/L), IR was water consumption rate (2 liters for adults and one for children's), ED was duration of vulnerability (70 years for adults and 10 years for children), EF was exposure frequency (365 days' years<sup>-1</sup>), BW was body weight (72 kg for adults and 32.7 kg for children), and AT was average life time (25,550 days for adults and 3650 days for children)<sup>[17,18]</sup>.

In this study, chronic and carcinogenic risk situation were evaluated. The HQ could be estimated by the following equation<sup>[16]</sup>.

$$HQ = ADD / RfD \quad (2)$$

In this equation, RfD- the toxicity reference dose was 0.0003 mg/kg.day<sup>[19]</sup>. If the HQ values were >1 the human health risk was exist<sup>[17,18,20]</sup>. The equation of cancer risk (CR) was as below:

$$CR = ADD \times CSF \quad (3)$$

The cancer slope factor (CSF) of EPA for As is 1.5 mg/kg.day<sup>[19]</sup>. The CR value greater than one in million (10<sup>-6</sup>) was generally considered significant by USEPA. All fixed coefficients and reference values from the literature in the calculations were used in µg/L.

## 3. Results and Discussion

### 3.1 Spatial Evaluation of Variation of Concentrations

To examine the temporal and spatial variation of arsenic, its concentrations between March 2015 and December 2021 were examined. Values between March 2015 and December 2019 were evaluated as pre-pandemic, and values between March 2020 and December 2021 were evaluated as post-pandemic.

When the values at the measurement stations before and after the COVID-19 pandemic were examined, it was seen that the concentrations at all stations increased, except for the 3rd Station. When the values before the pandemic were examined, it was seen that the highest concentration was 0.213 mg/L at the 10th Station and the lowest concentration was 0.0178 mg/L at the 1st Station. When the post-pandemic concentrations were examined, the highest concentration was again observed at the 10th Station (0.0358 mg/L), and the lowest concentrations were

observed at the 3rd (0.0189 mg/L) and 1st and (0.0193 mg/L) Stations. The mean and standard deviation values of As concentrations before and after the pandemic at the measurement stations were given in Table 2.

**Table 2.** The Mean and standard deviations of pre-pandemic and post pandemic As concentrations

Stations	Pre-Pandemic		Post-Pandemic	
	Mean	Std	Mean	Std
1	0.0178	0.0068	0.0193	0.0053
2	0.0206	0.0056	0.0218	0.0049
3	0.0194	0.0067	0.0189	0.0048
4	0.0195	0.0056	0.0201	0.0047
5	Not Enough Measurements		Not Enough Measurements	
6	0.0192	0.0059	0.0206	0.0046
7	0.0208	0.0063	0.0318	0.0272
8	0.0200	0.0074	0.0358	0.0373
9	0.0196	0.0074	0.0223	0.0060
10	0.0213	0.0066	0.0358	0.0314

It was thought that the reason for the decrease in the concentrations at the 3rd station after the pandemic was the decrease in the pollution load coming to the Eastern Wastewater Treatment Plant because of the decrease in the production in the industry during the pandemic. The general and seasonal averages of all values before and after the pandemic were examined. Accordingly, when the 7-year general averages are examined, it was seen that the highest concentration was 0.0256 mg/L at the 8th Station, and the lowest concentration is 0.0182 mg/L at the 1st Station. When the 7-year spring, summer and winter averages were examined, it was observed that all the maximum values were 0.0221 mg/L, 0.0231 mg/L and 0.0337 mg/L at the 7th Station, respectively. The maximum autumn average was determined as 0.0309 mg/L at the 8th Station. The minimum values in the spring, autumn and winter seasons were determined as 0.0187 mg/L, 0.0181 mg/L and 0.0170 mg/L at Station 1, respectively. The 7-year general and seasonal averages at the measurement stations were given in Table 3.

The reason why the highest value according to the 7-year averages was at the 8th station was that the wastewater of Nilüfer and Bursa Organized Industrial Zones was discharged to the Western Wastewater Treatment Plant before this station. The 1st Station, where the minimum concentration was, located in the upstream part of the Nilüfer Stream. The fact that the maximum values were found at the 7th and 8th Stations as a result of the seasonal evaluations shown that these organized industrial zones contribute to the pollution.

When all the pre- and post-pandemic values were analyzed by years and stations, the highest values were measured as 0.0457 mg/L and 0.0675 mg/L at the 10th and 8th Stations in 2020 and 2021, respectively. The minimum value was found to be 0.0127 mg/L at the 9th Station in 2018. The variation graph of the concentrations by years and stations was shown in Figure 2.

EPA and WHO recommended permissible limits for arsenic in drinking water were 0.05 mg/L and 0.01 mg/L, respectively [17,18]. When all stations were examined for 7 years, it was determined that all the values were above the WHO standard, and the annual average of the 8th Station in 2021 was above the EPA standard and all other values were below EPA Standards. Potable water standard value of Turkey (TSE266) was the same as WHO, and none of the measurement stations were in compliance with the Turkish Drinking Water standard [21].

The arsenic limit value allowed in irrigation water was 0.10 mg/L according to the WHO's irrigation water usage guide [22]. Turkish irrigation water standard value was

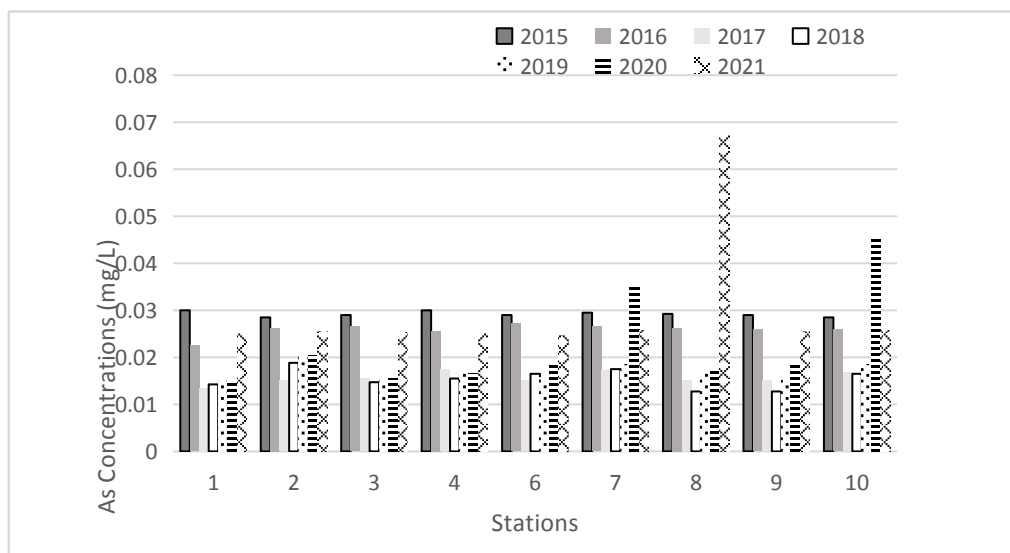
0.05 mg/L [23]. According to these values, Nilüfer Stream was found to be suitable for irrigation water in terms of As parameter. Only in 2021, the general average of the 8th Station was higher than the Turkish Irrigation Standard.

### 3.2 Evaluation of Human Health Risk

When the water quality of Nilüfer Stream was evaluated in terms of human consumption risk, it was determined that the hazard quotient (HQ) values were greater than 1 at all stations before and after the pandemic, and therefore there was a chronic and carcinogenic risk. Before the pandemic, the order of magnitude in the stations in terms of HQ values was  $10 > 7 > 2 > 8 > 9 > 4 > 3 > 6 > 1$ . The order of HQ magnitude in the stations of post-pandemic was  $8 > 10 > 7 > 9 > 2 > 6 > 4 > 1 > 3$ . In general, post-pandemic HQ values and risk had generally increased. A decrease was observed only at the 3rd Station. According to the values before and after the pandemic, it was observed that the 8th and 10th stations had a higher risk, and the 3rd and 1st stations had a lower risk than the other stations.

**Table 3.** General and seasonal means of 7 Years in the measurement stations

Seasons	Stations									
	1	2	3	4	5	6	7	8	9	10
7 Years mean	0.0182	0.0217	0.0195	0.0202		0.0206	0.0239	0.0256	0.0203	0.0213
7 Years Spring mean	0.0187	0.0201	0.0203	0.0209		0.0203	0.0221	0.0196	0.0197	0.0212
7 Years Summer mean	0.0192	0.0229	0.0213	0.0216	Not Enough Value	0.0210	0.0231	0.0210	0.0203	0.0190
7 Years Autumn mean	0.0181	0.0227	0.0204	0.0204		0.0214	0.0234	0.0309	0.0223	0.0234
7 Years Winter mean	0.0170	0.0214	0.0190	0.0193		0.0201	0.0337	0.0327	0.0190	0.0192



**Figure 2.** The variation graph of the concentrations by years and stations

The HQ order of the measuring stations was found as  $8 > 7 > 2 > 10 > 6 > 9 > 4 > 3 > 1$  according to the total 7-year averages before and after the pandemic. According to the post-pandemic and general average values, it could be said that the 8th Station had the highest risk, and the 3rd and 1st Stations had low risk.

When all HQ values were examined, it was seen that the highest value was 3.316 at Station 8 after the pandemic, and the lowest HQ value was at Station 1 before the pandemic with 1.615.

When the CR (carcinogenic risk) numbers were examined, it was hazardous for 7 years before and after the pandemic. After the pandemic, the values increased a little more. It was observed that the highest CR value was  $14924 \times 10^{-6}$  at the 8th Station after the pandemic, and the lowest was  $743 \times 10^{-6}$  at the 1st Station before the pandemic.

The 10th and 8th stations, where the concentrations were high, were located after the junction of the side streams and the discharge of Nilüfer and Bursa OIZs. Therefore, the pollution was more in there. The 1st Station was the upstream of the Stream, and the pollution sources were mixed later. Therefore, the health risk was found to be lower than the other stations. ADD, HQ and CR values calculated according to the general averages of 7 years before and after the pandemic were given in Table 4.

## 4. Conclusions

As a result of all the evaluations, it had been seen that Nilüfer Stream was not suitable for potable water quality according to National and International standards in terms of As parameter, but it was suitable for irrigation water quality.

After the pandemic, a decrease in pollution occurred, which was estimated to be due to the decrease in the production of the industrial zones located in the eastern part of the city only. However, pollution increased at all stations in other parts of the Stream. Therefore, the COVID-19 pandemic did not reduce As pollution. It had increased during the pandemic. It had been thought that the reason for this might be that the wastewater treatment plants did not carry out adequate treatment during the pandemic. Since the concentrations were higher than the standard values and a health risk in the upstream part where the point pollution sources were the least, it was shown that the pollution was not only caused by industry. It was also caused by the natural soil structure of the basin, mining activities and pesticide use. However, the increase in the concentration towards the downstream shown that the industry increased the pollution.

It was determined that the hazard quotient (HQ) values were greater than 1 at all stations before and after the pandemic.

**Table 4.** ADD, HQ and CR values calculated according to pre- and post-pandemic and 7-years general averages

Station	Pre-Pandemic			Post-Pandemic			Means of 7 years		
	ADD	HQ	CR	ADD	HQ	CR	ADD	HQ	CR
1	0.49537	1.6512	$743 \times 10^{-6}$	0.535714	1.785714	$804 \times 10^{-6}$	0.506667	1.688889	$760 \times 10^{-6}$
2	0.57197	1.9066	$858 \times 10^{-6}$	0.605556	2.018519	$908 \times 10^{-6}$	0.603395	2.011317	$905 \times 10^{-6}$
3	0.539352	1.7978	$809 \times 10^{-6}$	0.524306	1.747685	$786 \times 10^{-6}$	0.542088	1.806958	$813 \times 10^{-6}$
4	0.540509	1.8017	$811 \times 10^{-6}$	0.559524	1.865079	$839 \times 10^{-6}$	0.559722	1.865741	$840 \times 10^{-6}$
5	Not Enough Measurements								
6	0.534392	1.7813	$802 \times 10^{-6}$	0.572222	1.907407	$858 \times 10^{-6}$	0.571429	1.904762	$857 \times 10^{-6}$
7	0.576389	1.9213	$865 \times 10^{-6}$	0.883838	2.946128	$13258 \times 10^{-6}$	0.663105	2.210351	$995 \times 10^{-6}$
8	0.554167	1.8472	$831 \times 10^{-6}$	0.994949	3.316498	$14924 \times 10^{-6}$	0.710573	2.368578	$1066 \times 10^{-6}$
9	0.543056	1.8102	$815 \times 10^{-6}$	0.618056	2.060185	$92710 \times 10^{-6}$	0.564484	1.881614	$847 \times 10^{-6}$
10	0.590278	1.9676	$885 \times 10^{-6}$	0.993056	3.310185	$1489 \times 10^{-6}$	0.590278	1.967593	$885 \times 10^{-6}$

demic, and therefore there was a chronic and carcinogenic risk. Post-pandemic HQ values and risk had generally increased.

As a result, in order to prevent As pollution, it must to examine in detail the industrial (point) and agricultural (diffuse) pollutant sources originating from pesticide usage and to take protective measures. It must carry out the necessary inspections especially regarding the mining activities in the basin.

## Conflict of Interest

There is no conflict of interest.

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## ARTICLE

# Producing High Purity Nickel Metal Powder from Nickel Wastes through Acidic Leaching by Sulfuric Acid

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## ABSTRACT

Nickel has found increasing application in electronic, automobile manufacturing, plating, and metal industries and so on. Producing high quality metal powders to satisfy increasing demand for advanced materials is of very high importance. There are a few numbers of standard powder production techniques. An acidic leaching has been applied in present research. Sulfuric acid has been used to leach nickel wastes of plating industry. To produce nickel oxide powder furnaces with no protecting atmosphere and to produce pure nickel powder, tube furnace with hydrogen atmosphere has been applied. Variables performed in the research are time, density of sulfuric acid, and amount of hydrogen peroxide. To analyze powders produced, EDS element analysis and to determine size of powder particles, SEM has been applied. It was shown by the results that the highest amount of nickel dissolution in sulfuric acid (98%) has taken place during one hour and there is a direct relationship between hydrogen peroxide amount and nickel dissolution in sulfuric acid.

## 1. Introduction

Nickel as 24<sup>th</sup> metal element is one of the most frequent element available in earth's crust. Wide range usage made of nickel in different industries has led it to be considered as a strategic metal. In fact, this variety of application is resulted from various physical and chemical properties of this metal<sup>[1,2]</sup>. This is one of the important metals in industry and a basic one for modern technologies and industry. It is also important in energy, telecommunication, shape memory alloy, and electronics industries that are necessary

for economy, medical industry and or substructures<sup>[3,4]</sup>. Some studies have been performed in this respect which will be referred to.

Mansi et al.<sup>[5]</sup> with leaching of catalysts in a solution of 50% sulfuric acid, solid to liquid ratio 1:12 and in particle size less than 500 microns for 5 hours, at 100 °C with a stirring of 800 rpm, about 99% Recover of nickel. Oza et al.<sup>[6]</sup> used ultrasound to recover nickel from the catalysts along with the leaching method. In this work, they were able to extract about 95% of nickel from the text of nickel-alumina catalysts by nitric acid at a concentration

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of 40% at 90 °C and a solid to liquid ratio of 1:10 (g/mL) for 50 minutes. Using ultrasound, the recovery time was reduced from 7 hours to 50 minutes.

Randhawa et al.<sup>[7]</sup> conducted a study in which the leaching kinetics of nickel-cadmium batteries by sulfuric acid were investigated. Their results showed that the concentration of sulfuric acid up to 10% had a significant effect on the recovery of cadmium and nickel. However, nickel recovery was much lower than cadmium. Addition of hydrogen peroxide improved the nickel leaching kinetics, and nickel recovery increased to 96% at 5 hours of leaching, and nickel leaching also increased with increasing temperature. Driss et al.<sup>[8]</sup> used sulfuric acid and hydrochloric acid to recover nickel from palm oil catalysts. In this work, they investigated the effect of acid concentration parameters, solid to liquid ratio, temperature and leach time and found that sulfuric acid is more effective for nickel recovery. If the concentration of sulfuric acid is 67%, the leaching time is 140 minutes, the solid to liquid ratio is 1:14, about 60% of nickel will be recovered at 60 °C. If the temperature is above 80 degrees Celsius, this value will decrease.

In another study by Abrar et al.<sup>[9]</sup>, the recovery of nickel from a catalyst was investigated using the pressure dissolution method in nitric acid. The catalyst for this study is NiO/Al<sub>2</sub>O<sub>3</sub>, which is used for direct reduction and production of sponge iron. Results showed that at 140 °C maximum dissolution can be obtained but over this optimum temperature a reverse effect is noticed. Another important factor is the Rpm change effect, as a change from 600 to 300 caused a decrease of 10% of dissolution efficiency. Finally, it is shown that efficiency was improved when dissolution time increased.

Gharabaghi et al.<sup>[10]</sup> conducted a study entitled leaching kinetics of nickel extraction from hazardous scrap by sulfuric acid and optimization of dissolution conditions. It was found that nickel extraction increases with increasing sulfuric acid concentration, temperature and leaching time. Reducing particle size and solid to liquid ratio increased the dissolution of nickel. The extraction speed increased with increasing stirring speed and reached the highest level at 500 rpm. The maximum leaching rate was 97% at 25 °C after 30 minutes.

Liu and et al.<sup>[11]</sup> conducted research to produce high-purity basic nickel carbonate through chemical precipitation. They used electric double layer model to illustrate the adsorption mechanism of ions of sodium and chlorine and other impurities on solid surface. Experimental results indicate that the new process is very effective to remove Na<sup>+</sup> and Cl<sup>-</sup> to a level of both less than 0.01 wt%.

Li and et al.<sup>[12]</sup> also conducted research for the hydrothermal synthesis of nickel or cobalt-based carbonate hydroxides used in the production of supercapacitor electrodes. The results showed that the nickel-cobalt carbonate hydroxide electrode shows excellent cycling stability and is suitable for the production of supercapacitors.

In a study, Wu and et al.<sup>[13]</sup> produced nickel nanoparticles used in supercapacitors using hydrazine hydrate reduction. After conducting the experiment, nickel nanoparticles with a particle size of about 12 nm were obtained and they concluded that due to the good conductivity of nickel particles, it is a suitable option for producing supercapacitors. Huang and et al.<sup>[14]</sup> investigated the method by which nickel nanoparticles were produced. In this method, the production cost was reduced and nickel nanoparticles in the range of 180 nm to 260 nm were produced. They also controlled the size range of nickel particles by adjusting the reaction molar ratio and concentration. In one study, Li and et al.<sup>[15]</sup> produced ultrafine nickel powder and crystalline film using chemically controlled reduction. Their results showed that pure black nickel powder can be obtained when the pH > 10.0 and the temperature is in the range of 85 °C ~ 958 °C. RF plasma synthesis of nickel nanopowders via hydrogen hydroxide/nickel carbonate reduction was performed by Bai et al.<sup>[16]</sup>. They were able to produce nickel nanoparticles in the size range of 60 nm to 100 nm, which are used in the production of electrode materials.

Ultra fine nickel powder was produced by polyol method and its oxidation product by Zhou and et al.<sup>[17]</sup>. The results of this research showed that the high content of water in Ni(OH)<sub>2</sub> increases the reaction rate in the solution and decreases the average particle size of nickel powders. Paserin and et al.<sup>[18]</sup> investigated different methods for the mass production of nickel-based nanomaterials by the carbonyl process in a review article. In the research conducted by Alena and et al.<sup>[19]</sup>, the structure and properties of nickel nanoparticles prepared by selective leaching were investigated. They came to the conclusion that with this method it is possible to achieve a particle size of less than 5 nm and by increasing the temperature from 20 °C to 80 °C, the particle size will be in the range of 10 nm to 15 nm. Archana and et al.<sup>[20]</sup> conducted a research titled recovery of nickel powder from copper electrolyte by electrolysis. They were able to recover 87% of the nickel, which increased to 99% under certain conditions. The purity of the produced powder was 89.99%.

Since nickel powder is one of the basic and important metals in the industry, the production of this powder with high purity will be of special importance. After a lot of

research, we came to the conclusion that one of the important sources for the production of nickel powder is the use of nickel wastes, especially nickel wastes produced by electroplating. As shown in the research, one of the best methods for producing metal powder is the acid leaching method. For this reason, we decided to produce high-purity nickel powder, which is used in various industries, from nickel waste by acid leaching method, which will be fully explained in the following process.

## 2. Materials and Method

Main materials used in the research have been prepared from plating wastes. EDS analysis of the material is shown in Figure 1. For acidic leaching of the material also, sulfuric acid Merck (98 wt%) has been used.

Reaction times have been selected 5, 10, 20, 30, 40, 50, and 60 minutes; while, sulfuric acid concentrations have been 20%, 40%, 60%, 80%, and 98%. One of the methods to increase dissolution speed of nickel wastes in sulfuric acid is adding  $H_2O_2$  which effect of it has been studied through adding 50 cc, 100 cc, 150 cc, 200 cc, and 250 cc of the material. To stir and heat the solution in different stages of producing nickel powder, IKA/RCT basic hot plate stirrer (made in Germany) has been used. Producing nickel carbonate from nickel sulfate would be performed by sodium carbonate. Industrial type of sodium carbonate has been used in present research. To better perform the reaction between nickel sulfate and sodium carbonate, the temperature of the hot plate was set to 60 degrees Celsius. After finishing the reaction (Chemical reaction 2) and producing nickel carbonate, filter paper (Whatman) was used

to separate the solution from it. There is a possibility that there is sodium in the nickel carbonate, which requires a lot of washing to remove it, because sodium is soluble in water. To do so, distilled water has been used to produce nickel oxide and finally pure nickel, two different furnaces with controlling atmosphere have been required. In the research and to produce nickel oxide from nickel carbonate; ordinary furnace (AZAR-FURNACE M35L) with no controlling atmosphere has been used for one hour at 700 °C (Chemical reaction 3). Finally, a hydrogen Filled tube furnace (AZAR-FURNACE TF5/25) was used to convert nickel oxide into high purity nickel powder (Chemical reaction 4). The reduction process took place in two different cycles. The first cycle was performed at 700 °C for 2 hours and the second cycle at 600 °C for 4 hours. In general, production stages of nickel powder from nickel wastes include the four following stages:

Producing nickel sulfate from nickel wastes:  
 $(H_2SO_4 + Ni = NiSO_4 + H_2)$  (1)

Producing nickel carbonate from nickel sulfate:  
 $(NiSO_4 + Na_2CO_3 = NiCO_3 + Na_2SO_4)$  (2)

Producing nickel oxide from nickel carbonate:  
 $(NiCO_3 = NiO + CO_2)$  (3)

Producing high purity nickel powders from nickel oxide:  
 $(NiO + H_2 = Ni + H_2O)$  (4)

General production procedure of nickel powder is shown in Figure 2.

To determine EDS point analysis and to image produced powders, Vega/TSscan SEM (made in China) has been used. Minimum diameter of the device where the sample is contacted is 2 nanometers.

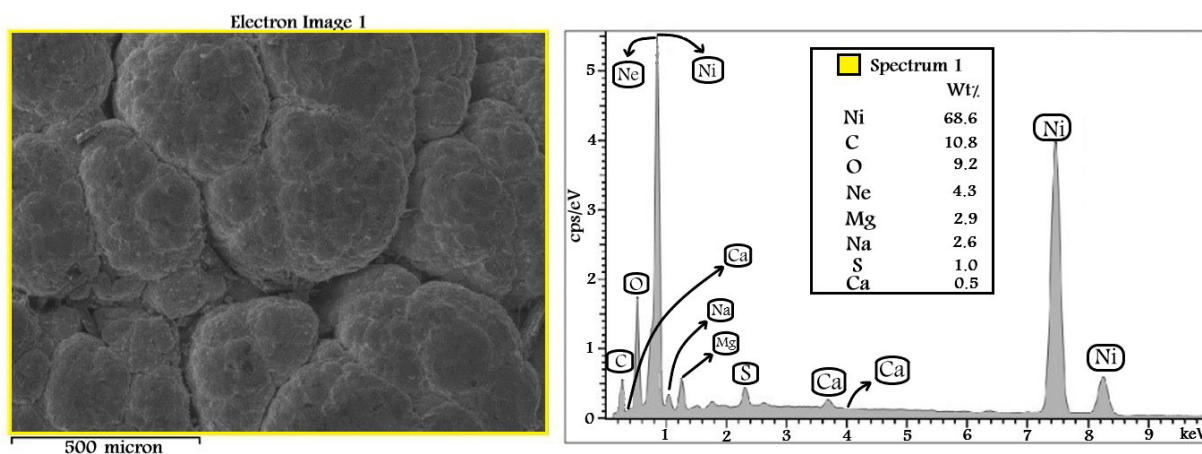


Figure 1. EDS analysis of wastes used in the research.

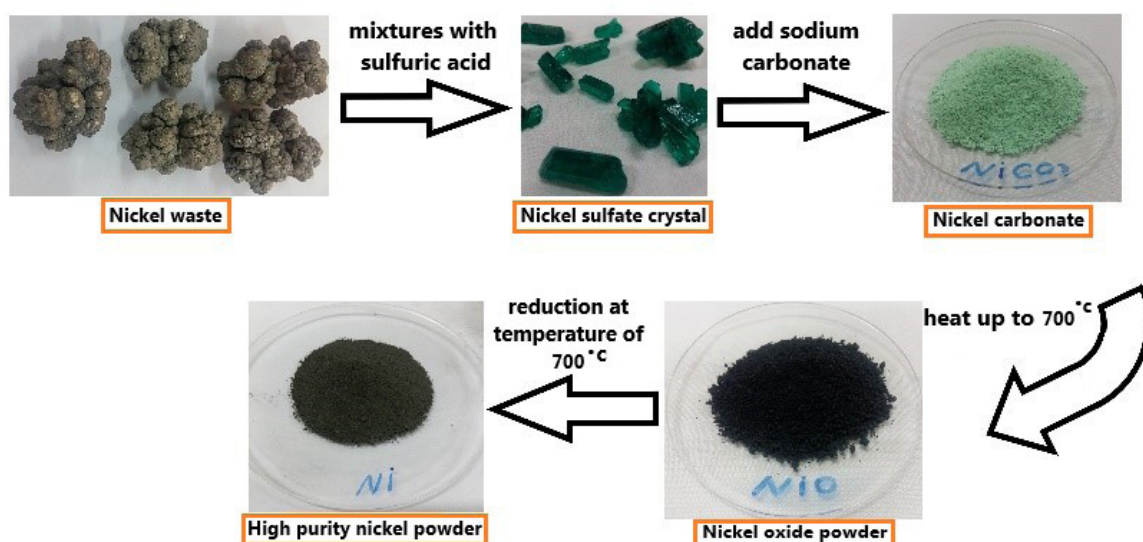


Figure 2. Flowchart of the research to produce high purity nickel powder.

### 3. Results and Discussion

After all four stages of producing nickel powder through acidic leaching, amounts of the product obtained in tests with final product have been computed and compared in reactions. In Table 1, the obtained have been compared with reaction stoichiometry reactions. At first stage, final product is nickel sulfate.

According to stoichiometry of the reaction, about 59.84 gr nickel would be dissolved in 100 gr sulfuric acid. The test and solving nickel waste in sulfuric acid has been performed for several times; and, nickel amount dissolved has been about 15 gr ~ 20 gr. End of the test has been considered to be at the point that no additional nickel would be dissolved in the solution and it would be considered as saturated. Final product of the second stage is nickel carbonate. According to the reaction stoichiometry, 68.48 gr sodium carbonate has to be consumed in each 100 gr of nickel sulfate so that the reaction would be complete;

and, finally, there would be 76.7 gr nickel carbonate. This amount of sodium carbonate used for produced nickel sulfate in the research is very high; because, less nickel has been dissolved in sulfuric acid, compared to stoichiometry. Therefore, different amounts of sodium carbonate have been tested. Finally, it became clear that 30 gr sodium carbonate is appropriate for each 100 gr of nickel sulfate solution and the reaction would be complete. Third and fourth stages are well matched with stoichiometry. High difference in stages one and two can be due to type of nickel wastes used as well as purity of acid. Numbers obtained in stoichiometries reactions' will consider all conditions as ideal which their performance would be very hard and sometimes impossible in practical and lab conditions.

As referred to in the Research Materials and Method, one of the most important parameters in increasing dissolution of nickel wastes is sulfuric acid concentration, time and amount of hydrogen peroxide. The results obtained

Table 1. Comparing reaction products obtained in the research through stoichiometry.

Stage number	Final product	Final weight of the product in the laboratory	Final product weight according to stoichiometry	Difference (%)
1	NiSO <sub>4</sub>	52.73	157.78	66.5
2	NiCO <sub>3</sub>	33.6	76.7	56.2
3	NiO	61.36	62.92	2.46
4	Ni	77.17	78.57	1.27

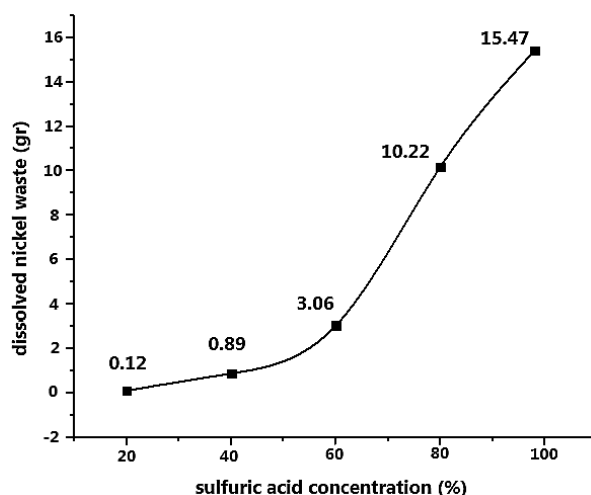
from effect of these three parameters in dissolution of nickel wastes in sulfuric acid would be presented in this paper. Figure 3 shows effect of sulfuric acid concentration on amount of nickel wastes' dissolution. The test for all concentrations has been performed during one hour. As shown in the above figure, through increase of sulfuric acid concentration, dissolution amount of nickel wastes would be increased. At 20% and 40% concentrations, dissolution amount is very low and there is no main difference between the two concentrations; however, at 60% to 98% concentrations, a steep slope would be created in dissolution of nickel wastes. This shows that sulfuric acid with concentrations more than 60% can end to acceptable results.

In continuation of studying parameters, effect of reaction time duration has been dealt with. The test has been performed in sulfuric acid (98%), showing the highest efficiency in terms of dissolution in previous section. The results are provided in Figure 4. Figure 4 showed that, through increase of dissolution process time, more nickel wastes have been dissolved in sulfuric acid. This dissolution would be continued till saturation of the solution.

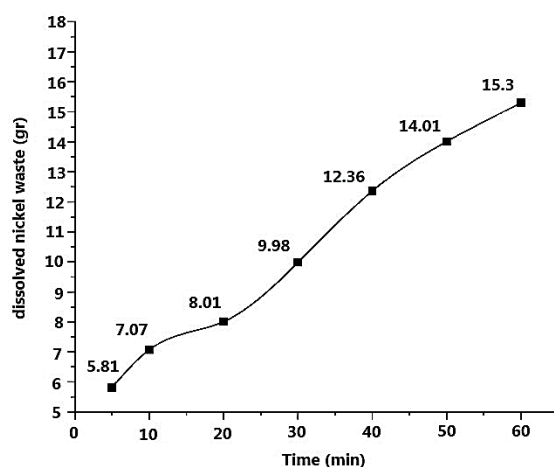
Another important parameter studied was the effect of amount of hydrogen peroxide on amount of dissolution (Figure 5). The test has been performed during one hour dissolution time in sulfuric acid (98%).

It became clear that adding hydrogen peroxide has a positive effect in increasing dissolution of nickel wastes in sulfuric acid. The reason for increased dissolution is increased oxidation and activation of surface of nickel wastes. As shown by the results, in previous test and during one hour 15.3 gr nickel wastes have been dissolved in sulfuric acid (98%). This amount has been increased to 16.91 gr after adding 50 cc hydrogen peroxide to the solution, through increasing of hydrogen peroxide to the solution, dissolution amount of nickel wastes also has been increased. To study purity of nickel powder produced in the research, EDS element analysis has been performed on powders (Figure 6).

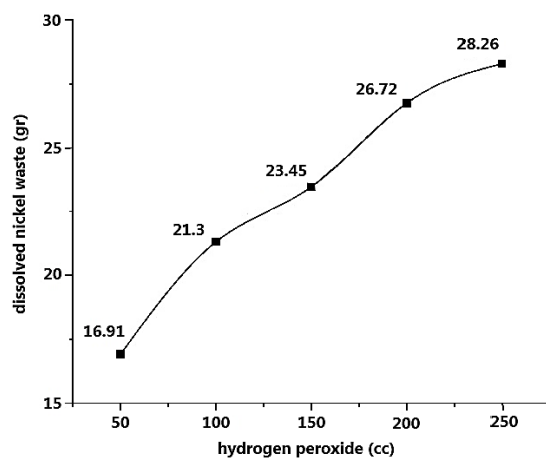
Nickel powder produced is of 99.6% purity which is high; however, existence of 0.4% of sulfur in analyses of powders can be due to following reasons: firstly, in initial analysis of nickel wastes there is about 1% sulfur which has been remained till the final stage of powder production. Secondly, the reason justifying this amount of sulfur goes back to the first stage of nickel powder production and preparation of nickel sulfate through sulfuric acid. To study shape of nickel powder particles produced, images from SEM are shown in Figure 7.



**Figure 3.** Effect of sulfuric acid concentration in dissolution of nickel wastes.



**Figure 4.** Effect of reaction time duration on dissolution of nickel wastes.



**Figure 5.** Effect of amount of hydrogen peroxide on dissolution of nickel wastes.

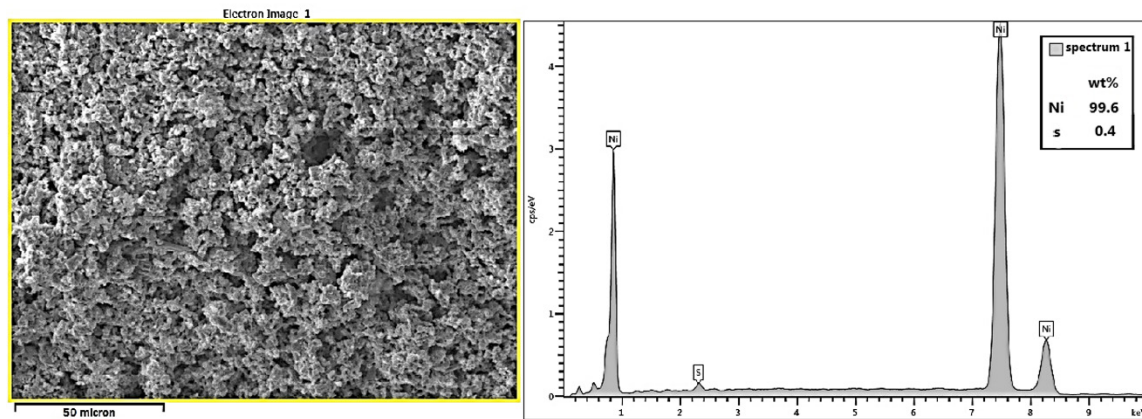


Figure 6. EDS element analysis performed on produced nickel powder.

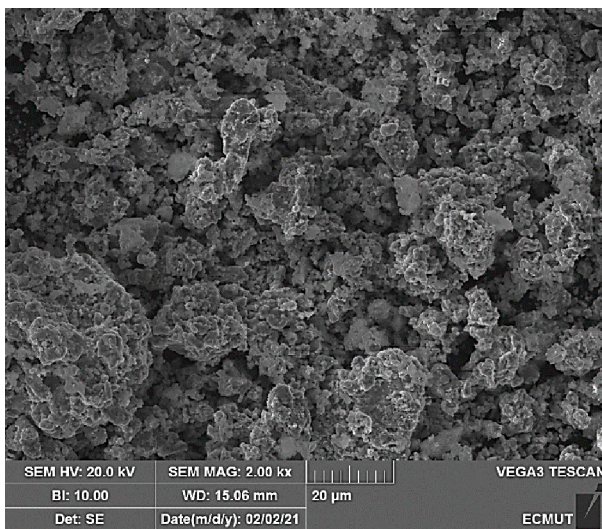


Figure 7. SEM images from nickel powder produced.

It can be suggested that powder particles produced had porous and irregular shape. To determine size distribution of produced powder particles, sifting is one of the common methods. To do so, 80 gr of nickel powder has been separated and passed through screen to determine size of particles. Size distribution of powder particles is shown in Figure 8.

The highest distribution is related to the range of 44 microns ~ 74 microns. Size of powder particles during third and fourth stages related to production of nickel oxide and pure nickel can be controlled. If at reduction stage of powders, temperature would be reduced and time would be increased; lower size of particles would be resulted. Therefore, the reduction temperature was 600 °C and the time was 4 hours. Elemental analysis (EDS) of nickel powder produced was performed after the completion of this cycle (Figure 9). As shown in the Figure 9, the nickel analysis shows a value of 100%.

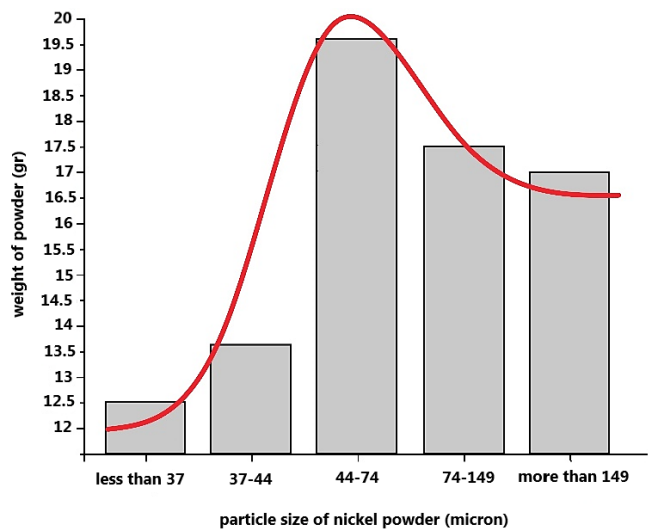


Figure 8. Size distribution of nickel powder produced in the research.

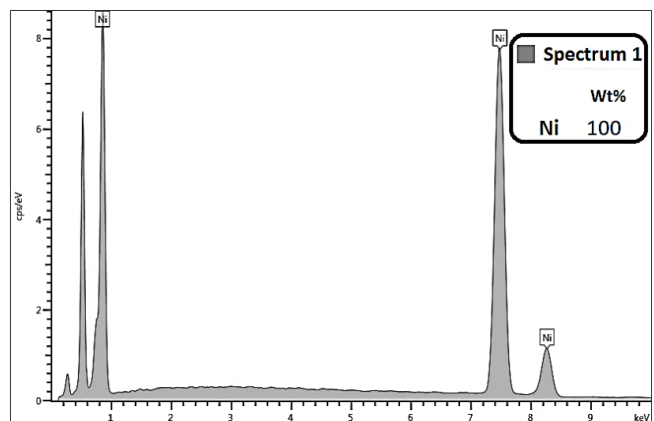
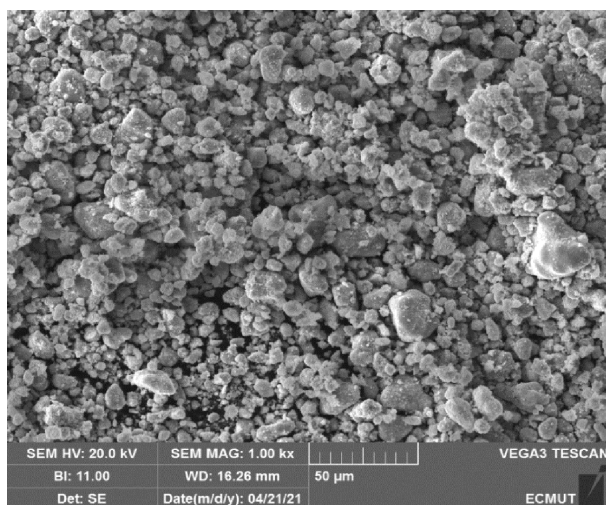
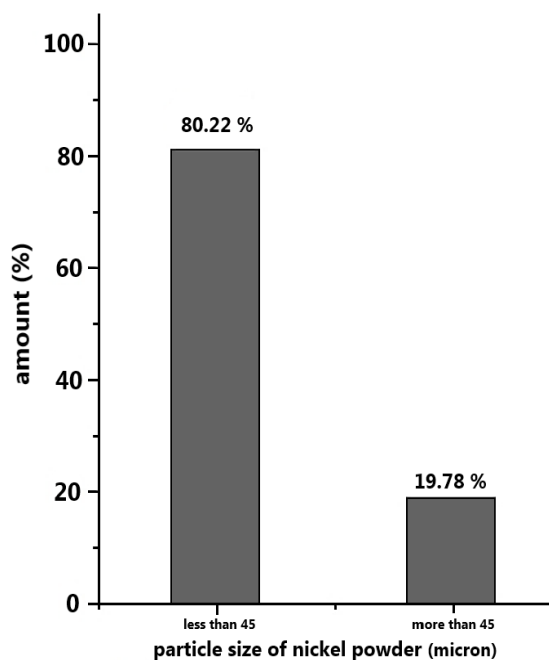


Figure 9. Elemental analysis (EDS) of nickel powder after a cycle of 600 °C and a time of 4 hours.

SEM images were also obtained from samples of powders produced in this cycle (Figure 10). Due to this shape and compared to the sample of powders produced from the previous cycle and Figure 7, the produced powders were much finer. The dispersion of the powder particle size produced in the second cycle was measured (Figure 11). According to this figure, 80.22% of the produced powders were less than 45 microns.



**Figure 10.** SEM image of nickel powder produced after the second reduction cycle.



**Figure 11.** Nickel powder particle size dispersion after the second reduction cycle.

#### 4. Conclusions

Acidic leaching to produce high purity nickel powder

from nickel wastes through sulfuric acid has been performed in the research and the results are as follows:

1) The two parameters of sulfuric acid concentration and duration of process have had a direct effect on dissolution of nickel wastes in sulfuric acid. That is, upon increase of acid concentration from 20% to 98%, dissolution amount of nickel wastes has been increased from 0.12 gr to 15.47 gr. Also, upon increasing of time from five to 60 minutes, dissolution amount of nickel wastes has been increased from 0.81 gr to 15.3 gr.

2) Hydrogen peroxide ( $H_2O_2$ ) has been considered as one of the main and important factors in increasing dissolution of nickel wastes in sulfuric acid. That is during one hour fixed, 15.3 gr ~ 15.47 gr of nickel wastes have been dissolved in the solution with no hydrogen peroxide; however, adding 50cc of hydrogen peroxide during the same time has led to increase of nickel wastes' dissolution to about 16.91 gr. This is about 10% higher than the time no hydrogen peroxide has been used. In industrial scale, it is considered as a considerable amount. In general and upon increase of hydrogen peroxide, dissolution amount of nickel wastes also has been increased due to surface of nickel wastes becoming activated.

3) Nickel powder produced through acidic leaching has been highly pure. Elemental analysis (EDS) of this powder in the first reduction cycle (temperature 700 °C and time 2 hours), showed 99.6%, which is considered as an acceptable purity. Also, particles of nickel powder have been porous and irregular. Size range of nickel powder has been computed and maximum value has been related to size of particles within the range of 44 microns ~ 74 microns.

4) After the second reduction cycle (temperature of 600 °C and time of 4 hours), elemental analysis of the produced nickel powder showed 100%. Also, after this cycle, the particle size of nickel powder became smaller than the first cycle. Most of the particle size dispersions were obtained in the range below 45 microns.

#### Conflict of Interest

There is no conflict of interest.

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## REVIEW

# Anti-bacterial Properties of Transition Metal Complexes of Copper Metal Ion: A Mini Review

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## ABSTRACT

Bacterial infections are a major cause for impulsive deaths in human beings. Bacterial infections of the respiratory, gastrointestinal and central nervous system account for the majority of cases of sudden casualties. Readily available drugs are getting ineffective by each passing day as the mutation is very fast in these pathogenic microbes resulting in drug resistance. The growing resistance of bacteria necessitates the development of new and effective compounds of desired characteristics that could bar the rapid development of bacterial cell inside of the host body. Along with cellular resistance for clinical antibiotics, co-bacterial infections during microbial attacks (*viz.* virus, fungus, protozoans etc.) also demand for some novel antibacterial drugs having high efficacy and minimal side effects on human body. These antibiotics should also be compatible with remedies ongoing for core microbial infections. So, in demand of search for effective antibacterial moieties, the scope of transition metal complexes as drug gives a good signal against the pathogenic bacteria by inhibiting their growth. The action of metal complexes on bacterial cell may be due to impermeability, enzymatic interruptions, ribosomal interactions, disturbance in the path of protein synthesis, denaturing of genetic materials etc. inside the cell. Metals in complexes may interrupt the lipophilicity through the bacterial cell wall. Inclusion of metal ions in organic moieties behaving as ligand delocalize  $\pi$ -electrons upon the entire chelate ring and this chelation results in overlapping of ligand orbital and partial sharing of (+)ve charge of metal ion with donor atoms. These structural modifications in metal and organic lone pair donor species are the supposed reasons for their enhanced antimicrobial activities against pathogenic microbes. The present review focuses on the impact of recently synthesized, well characterized mono and binuclear transition metal complexes of Cu ions that have the potential to be the drug of the decade in medicinal inorganic chemistry for treating the bacterial diseases.

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## 1. Introduction

Discovery of *cis*-platin opened the door for the exploration of an enormous number of other biologically active metal complexes<sup>[1,2]</sup>. It was then a new interest of the pioneer to synthesize novel transition metal complexes. Transition metals complexes with metal ion/s and a variety of ligands developed from organic and/ or inorganic moieties were of interest of chemists for the structural elucidation and their applications in various emerging field of science and technology<sup>[3,4]</sup>. Transition metal complexes have shown their importance in all the area of chemistry serving to society<sup>[5-7]</sup>. Among different applications, metal complexes are studied as potent drug molecules against many day to day life diseases to lethal diseases, viz. general microbial infections, diabetes, inflammation, cancer, acquired immune deficiency syndrome, Alzheimer, Parkinson etc. Among various therapeutic potentials, antimicrobial applications of metal complexes are the centre of attention for medicinal chemists due to resistance of pathogenic microbes against traditional antibiotics developed from organic synthons<sup>[8-10]</sup>. Copper was known well for its anti-microbial as well as therapeutic properties from a very long time<sup>[11]</sup>. Now, its ionic complexes are studied as drugs in modern medical sciences and are of interest among medicinal chemists for evaluating drug likeness behaviour against various lethal diseases<sup>[12-16]</sup>. In recent years, copper metal ions became very popular along with other transition metal ions for the study of antibacterial properties along with antifungal and anticancer properties of transition metal complexes on both Gram positive and Gram negative bacteria and other microbes and cancer lining cells, respectively<sup>[14,17-37]</sup>. In the current pandemic of COVID-19, many metal complexes including copper have been tested and found effective against various strains of corona virus by *in silico* mean<sup>[12,13]</sup>. Transition metal complexes of copper metal ions on a variety of ligands have shown promising results on pathogenic Gram positive bacteria such as *S. aureus*, *B. subtilis*, *E. Faecalis*, *S. mutans*, *S. gordonii*, *B. cereus* and Gram-negative bacteria such as *E. coli* and *S. typhi*, *P. aeruginosa* and *K. pneumonia*, *V. cholera* and *S. pneumonia*<sup>[17-20]</sup>. The final activities of different transition metal complexes of copper ions are different on tested organisms as it largely depends on either the impermeability of cells of organisms or the difference in the ribosome of bacterial cells as well as on the nature of ligands used to prepare the complexes<sup>[38-43]</sup>. In the present review, we tried to set a view of antibacterial efficacy of copper based metal complexes in front of global researchers to drag their attention for further discoveries and researches to find copper metal complexes as potent antibacterial medicinal agent.

## 2. Historical Developments for Antibacterials

The treatment of bacterial infections approved by administration of chemotherapeutic agents, the therapy was began in the 1930s, and was one of the most profound medical advances occurred in twentieth century. All the antibacterial drugs in clinics today were developed by drug discovery programmes and systematic studies leads to identify inhibitors by tracing their mode of action and ability to prevent bacterial growth. The ‘golden period’ of antibacterial-drug discovery was laid between the 1940s and 1970s<sup>[44,45]</sup>. The development of these therapeutics or agents derived from them helped a lot to combat the disease burden. In the meanwhile the emergence of resistance to antibiotics in pathogenic bacteria worldwide during the past three decades threatened the public health globally and challenged the medicinal chemist profoundly. This could destabilize the major advances achieved in the treatment of infection so far<sup>[46-49]</sup>. The developments in molecular modelling, bioinformatics, biochemistry and target-based drug discovery program advances the current strategy for finding and develop therapeutics as antibacterial. Though molecular targets for effective antibacterials are fairly few but they are found to involve consistently in the pathways of macromolecular synthesis. They are indeed, the essential components and comprise for functioning of bacteria that cannot be satisfied by providing intermediates. Especially, very few targets of the major classes of antibacterials used in systemic mono-therapy are essential enzymes present in bacterial cell. Some clinical antibacterial drugs used as reference in antibacterial evaluation of metal complexes are listed in Table 1 along with their IUPAC name and chemical structure.

## 3. Antibacterial Activity of Mononuclear Copper Complexes

Some of the considerable mononuclear copper metal complexes on different ligands were synthesized and screened for their anti-microbial and anti-tumour activities. Transition metal complexes of copper such as  $[\text{Cu}(\text{L}_1)_2] \cdot 2\text{H}_2\text{O}$ ,  $[\text{Cu}(\text{L}_2)_2] \cdot 2\text{H}_2\text{O}$ ,  $[\text{Cu}(\text{L}_3)_2] \cdot 2\text{H}_2\text{O}$ ,  $[\text{Cu}(\text{L}_4)_2] \cdot 2\text{H}_2\text{O}$  have been prepared by deprotonation of Schiff base ligands ( $\text{HL}_1$ – $\text{HL}_4$ ) designed by condensation of 4-Fluorobenzylamine with 2-Hydroxy-1-naphthaldehyde/3,5-Dichlorosalicylaldehyde/3,5-dibromosalicylaldehyde/3-Bromo-5-chlorosalicylaldehyde. All of these metal complexes were characterised using different physiochemical techniques and the spectro analytical data favours well the proposed structure of synthesized ligands and metal complexes<sup>[19]</sup>. Also *in vitro* screening of these well screened ligands and metal complexes of Cu

**Table 1.** Chemical structure and IUPAC name of some antibacterial drugs taken as standard/ control during in vitro antibacterial activity screening of ligands and metal complexes.

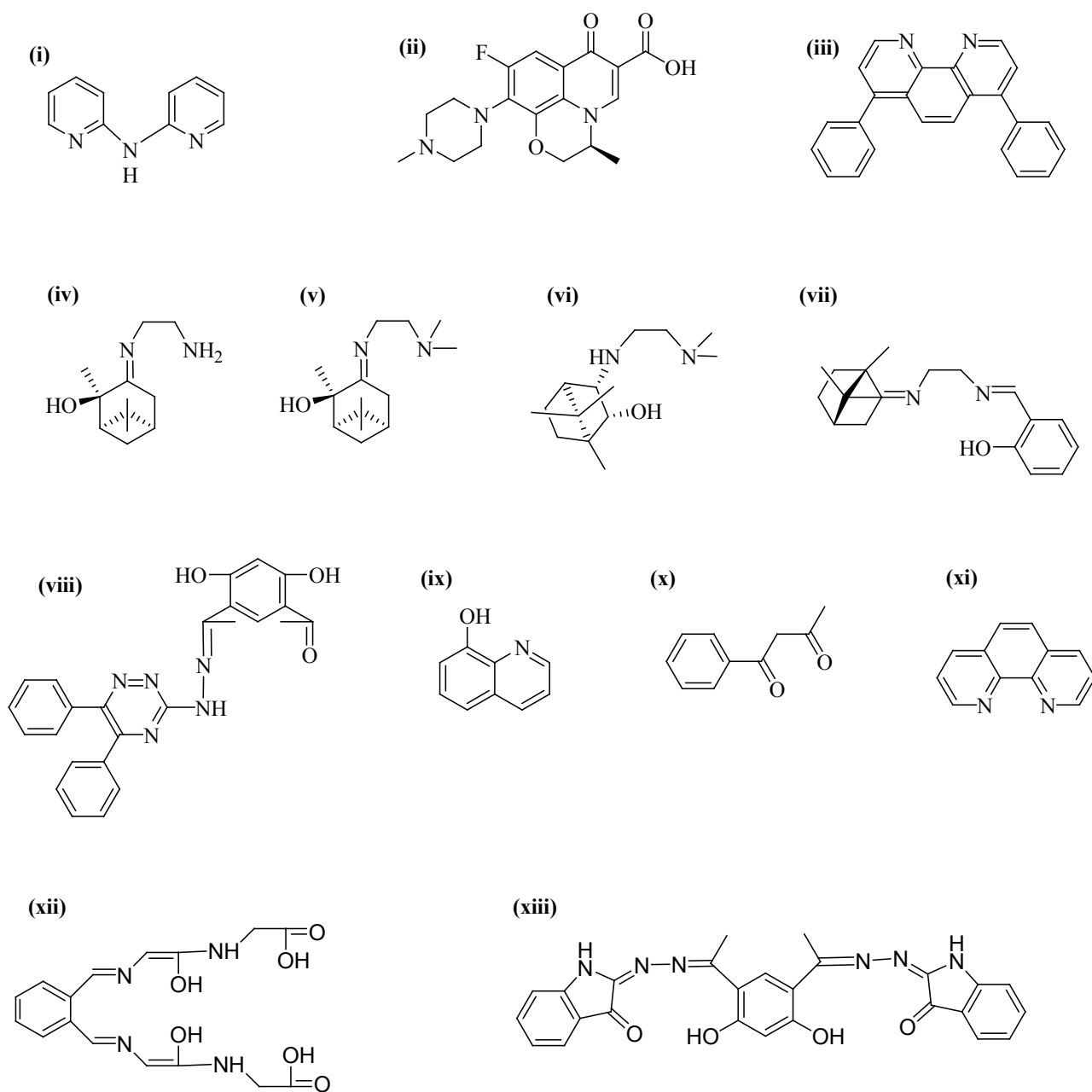
S.N.	Drug	Chemical structure	IUPAC Name	Ref.
1	Ciprofloxacin		1-Cyclopropyl-6-fluoro-4-oxo-7-piperazin-1-yl-1,4-dihydroquinoline-3-carboxylic acid	[50]
2	Furacilinum / Furacine		[(E)-(5-nitrofuran-2-yl)methylideneamino]urea	[50]
3	Doxycycline		(4S,4aR,5S,5aR,6R,12aR)-4-(dimethylamino)-1,5,10,11,12a-pentahydroxy-6-methyl-3,12-dioxo-4a,5,5a,6-tetrahydro-4H-tetracene-2-carboxamide	[50]
4	Norfloxacin		1-ethyl-6-fluoro-4-oxo-7-piperazin-1-ylquinoline-3-carboxylic acid	[50]
5	Ampicillin		(2S,5R,6R)-6-[[[(2R)-2-amino-2-phenylacetyl]amino]-3,3-dimethyl-7-oxo-4-thia-1-azabicyclo[3.2.0]heptane-2-carboxylic acid	[51]
6	Chloramphenicol		2,2-dichloro-N-[(1R,2R)-1,3-dihydroxy-1-(4-nitrophenyl)propan-2-yl]acetamide	[51]
7	Levofloxacin		(2S)-7-fluoro-2-methyl-6-(4-methylpiperazin-1-yl)-10-oxo-4-oxa-1-azatricyclo[7.3.1.0.5,13]trideca-5(13),6,8,11-tetraene-11-carboxylic acid	[50]
8	Streptomycin		2-[(1R,2R,3S,4R,5R,6S)-3-(diaminomethylideneamino)-4-[(2R,3R,4R,5S)-3-[(2S,3S,4S,5R,6S)-4,5-dihydroxy-6-(hydroxymethyl)-3-(methylamino)oxan-2-yl]oxy-4-formyl-4-hydroxy-5-methylloxolan-2-yl]oxy-2,5,6-trihydroxycyclohexyl]guanidine	[51]
9	Chlorhexidine		(1E)-2-[6-[[[amino-[(E)-[amino-(4-chloroanilino)methylidene]amino]methylidene]amino]hexyl]-1-[amino-(4-chloroanilino)methylidene]guanidine	[50]
10	Gentamycin		(2R,3R,4S,5R)-2-[(1S,2R,3S,4S,6S)-4,6-diamino-3-[(2S,3S,6S)-3-amino-6-[(1S)-1-(methylamino)ethyl]oxan-2-yl]oxy-2-hydroxycyclohexyl]oxy-5-methyl-4-(methylamino)oxane-3,5-diol	[51]

yielded some fruitful results when tested against Gram positive *S. gordonii* and *S. aureus* and Gram negative *E. coli* and *P. aeruginosa* with Ciprofloxacin as a standard reference.  $[\text{Cu}(\text{L}_3)_2] \cdot 2\text{H}_2\text{O}$  showed the most promising results against Gram positive while  $[\text{Cu}(\text{L}_4)_2] \cdot 2\text{H}_2\text{O}$  showed the most promising result against Gram-negative under laboratory conditions among other metal complexes used in this screening process<sup>[19]</sup>. Copper complexes of formulae  $[\text{Cu}(\text{L}_3)_2] \cdot \text{H}_2\text{O}$ ,  $[\text{Cu}(\text{Br})(\text{L})] \cdot \text{H}_2\text{O} \cdot \text{CH}_3\text{OH}$ ,  $[\text{Cu}(\text{L})\text{Cl}] \cdot \text{C}_2\text{H}_5\text{OH}$  of ligand 1-phenyl-3-methyl-4-benzoyl-5-pyrazolone-4-ethylthiosemicarbazone were prepared, purified and screened against Gram positive bacteria *B. cereus* and *S. aureus* and Gram negative *S. abony* using Furacilinum as the standard reference<sup>[20]</sup>. In results, the metal complexes appeared to be impactful against screened bacteria<sup>[20]</sup>. Transition metal complex  $[\text{Cu}(\text{L})_2]$  of crystal X-ray studied ligand 1-(2-nitrobenzylidene)-2-(phthalazin-1-yl)hydrazine was synthesized and characterized by spectral and physical methods viz. IR, UV-vis., NMR, Mass, TGA etc. and then tested for its antibacterial activity against Gram positive *E. faecalis*, *S. mutans* and *S. aureus* and Gram negative *E. coli*, *P. aeruginosa* and *K. pneumoniae* taking Ciprofloxacin as the standard reference drug and the inhibition capacity of the metal complex, in this case, is accordingly to the inhibition of the ciprofloxacin<sup>[18]</sup>. Organic ligandsamidino-O-methylurea ( $\text{L}^1$ ), N-(benzyl)-amidino-O-methylurea ( $\text{L}^2$ ), 2,2'-bipyridine (bipy) and 1,10-phenanthroline (phen) were applied to produce a series of mixed ligand copper complexes with formulae  $[\text{Cu}(\text{L}^1)(\text{bipy})] \cdot \text{Cl}_2$ ,  $[\text{Cu}(\text{L}^1)(\text{phen})] \cdot \text{Cl}_2$ ,  $[\text{Cu}(\text{L}^2)(\text{bipy})\text{Cl}_2]$  and  $[\text{Cu}(\text{L}^2)(\text{phen})] \cdot \text{Cl}_2$  possessing antibacterial properties. Antibacterial potency order of tested complexes were predicted as  $[\text{Cu}(\text{L}^1)(\text{phen})] \cdot \text{Cl}_2 > [\text{Cu}(\text{L}^2)(\text{phen})] \cdot \text{Cl}_2 > [\text{Cu}(\text{L}^1)(\text{bipy})] \cdot \text{Cl}_2 > [\text{Cu}(\text{L}^2)(\text{bipy})\text{Cl}_2]$  against three Gram negative bacterial strains *E. coli*, *Salmonella* and *Campylobacter*. The best inhibition action was performed by  $[\text{Cu}(\text{L}^1)(\text{phen})] \cdot \text{Cl}_2$  against *Campylobacter*<sup>[52]</sup>. Well characterized copper (I) halide complexes  $[\text{Cu}(\text{L}^1)_2\text{Cl}]$ ,  $[\text{Cu}(\text{L}^1)_2\text{Br}]$ ,  $[\text{Cu}(\text{L}^1)_2\text{I}]$ ,  $[\text{Cu}(\text{L}^2)_2\text{Cl}]$ ,  $[\text{Cu}(\text{L}^2)_2\text{Br}]$ ,  $[\text{Cu}(\text{L}^3)_2\text{Br}]$  coordinated with S atoms of thiocarbamide fragments of 4-thioxo[1,3,5]oxadiazocines ligands ( $\text{L}^1$ - $\text{L}^3$ ) were evaluated for their antibacterial potential via bioluminescent toxicological assay against *E. Coli* K12 TG1 bacterial strain and results were compared with free ligands and standard antibacterial drugs Doxycycline, Norfloxacin, Ciprofloxacin, Ampicillin and Chloramphenicol. The complexes of  $\text{L}^1$  and  $\text{L}^2$  ligands occupied with electron dragging groups showed stronger activity comparable activity to reference drugs against targeted microbial strain<sup>[53]</sup>. Bioactive Cu(II) mixed ligand complexes  $[\text{Cu}(\text{Lv}_x)(\text{Dpya})\text{Cl}] \cdot \text{Cl}$

and  $[\text{Cu}(\text{Lv}_x)(\text{Dphen})\text{Cl}] \cdot \text{Cl}$  of commercial antibiotic levofloxacin ( $\text{Lv}_x$ ) with 2,2'-dipyridylamine (Dpya) and 4,7-Diphenyl-1,10-phenanthroline (DPhen), respectively [Figure 1: i, ii, iii (ligands); Figure 2: 1, 2 (complexes)] were reported active against four Gram positive *S. aureus*, *B. subtilis*, *E. faecalis* and *S. pneumoniae* and five Gram negative *P. mirabilis*, *S. flexneri*, *E. coli*, *Citrobacter* species and *S. typhi* bacterial cells. Antibacterial activity was evaluated *in vitro* by disc diffusion method in agar media as nutrient and results were compared with levofloxacin as parent ligand and neomycin as reference drug. Antimicrobial activity data obtained clearly indicate that inhibition potential of both copper complexes is much higher than the free levofloxacin and metal salt tested against targeted bacterial strains<sup>[54]</sup>. Methicillin resistant bacteria *S. aureus* and *P. aeruginosa*, *E. coli*, *M. vaccae*, *B. subtilis* pathogenic bacterial strains were targeted to evaluate antibacterial efficacy of four novel copper complexes with chiral properties synthesized from terpene derived ethane-1,2-diamine ligand [Figure 1: iv, v, vi, vii (ligands); Figure 2: 3, 4, 5, 6 (complexes)]. Structural elucidation of prepared compounds was done with the help of advance physico spectral techniques and well supported as proposed. IR and NMR data revealed bidentate behaviour of ligands iv-vi, while the ligand viii acts as tridentate in coordination with copper metal ions. The *in vitro* antibacterial potential of all copper complexes was reported comparable to the standard medicine ciprofloxacin used as reference drug<sup>[55]</sup>. Gram positive *S. aureus*, *B. subtilis* and Gram negative *E. coli*, *S. typhimurium* bacterial strains were targeted by mononuclear complexes (7-14) of acetate, chloride, nitrate, sulphate salts of copper metal ion with a novel hydrazone ligand and/or 8-hydroxyquinoline, 1,10-phenanthroline, benzoylacetone as mixed ligands [Figure 1: viii( $\text{H}_2\text{L}^1$ ), ix(HQ), x(Bac), xi(Phen) ligands; Figure 2: 7, 8, 9, 10, 11, 14 (complexes)]. Antibacterial activity data, *in vitro*, indicate that the ligand and their metal complexes;  $[(\text{HL}^1)\text{Cu}(\text{OAc})(\text{H}_2\text{O})] \cdot 1.5\text{H}_2\text{O}$  (7),  $[(\text{H}_2\text{L}^1)\text{Cu}(\text{SO}_4)(\text{H}_2\text{O})_2] \cdot 1.5\text{H}_2\text{O}$  (8),  $[(\text{HL}^1)\text{Cu}(\text{H}_2\text{O})_3] \cdot \text{Br} \cdot \text{H}_2\text{O}$  (9),  $[(\text{HL}^1)\text{Cu}(\text{HQ})(\text{H}_2\text{O})]$  (10),  $[(\text{HL}^1)\text{Cu}(\text{H}_2\text{O})(\text{Bac})] \cdot 2\text{H}_2\text{O}$  (11) showed a buoyant activity against the Gram positive bacteria; *B. Subtilis*, but complexes  $[(\text{HL}^1)\text{Cu}(\text{H}_2\text{O})] \cdot \text{NO}_3$  (12),  $[(\text{HL}^1)\text{CuCl}] \cdot 1.5\text{H}_2\text{O}$  (13),  $[(\text{HL}^1)\text{Cu}(\text{OAc})(\text{Phen})]$  (14) showed no effect even. Targeted strains of *S. aureus*, *E. coli*, and *S. typhimurium* were unaffected by test compounds  $\text{H}_2\text{L}^1$  and all copper complexes<sup>[56]</sup>. 2-cetylpyridinenicotinichydrazone; HL as ligand applied to synthesize copper complexes as  $[\text{Cu}(\text{L})_2]$ ,  $[\text{Cu}(\text{HL})\text{Cl}_2]$  and  $[\text{Cu}(\text{HL})\text{Br}_2]$  in 1:2, 1:1 and 1:1 metal ligand ratio (M : L), respectively. These complexes were well characterized by single X-ray crystallography along with IR, UV-vis., NMR and

Mass spectral techniques. Spectral studies supported well the proposed structure, coordination mode and geometry of copper complexes. These complexes and ligand were studied for the evaluation of in vitro antibacterial potential against *S. mutans*, *S. mitis*, *S. sanguinis*, *S. sobrinus*, *L. casei*, *S. salivarius* and *E. faecalis* bacterial strains. Min-

imum inhibitory concentration of dilutions of ligands and complexes were observed and compared with Chlorhexidine as standard antibacterial drug. The minimum inhibitory concentration data showed the enhanced activity of complexes than free ligand and satisfactory as compared to standard control drug <sup>[57]</sup>.



**Figure 1.** Structure of some antibacterial ligands (i-xiii) applied to prepare copper complexes <sup>[53-56]</sup>

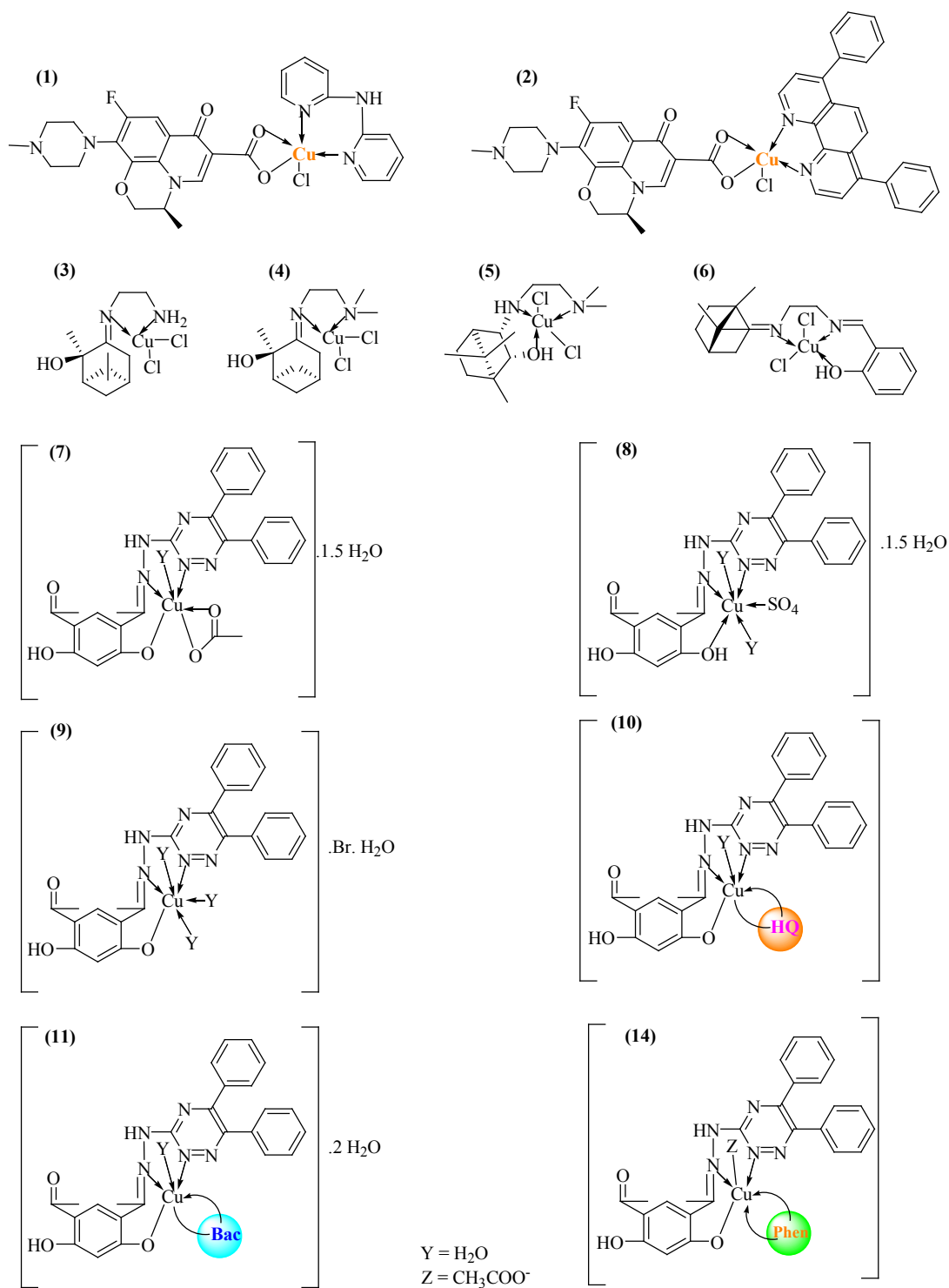


Figure 2. Structure of antibacterial copper complexes (1-11, 14) of ligands (i-vii) <sup>[53-56]</sup>

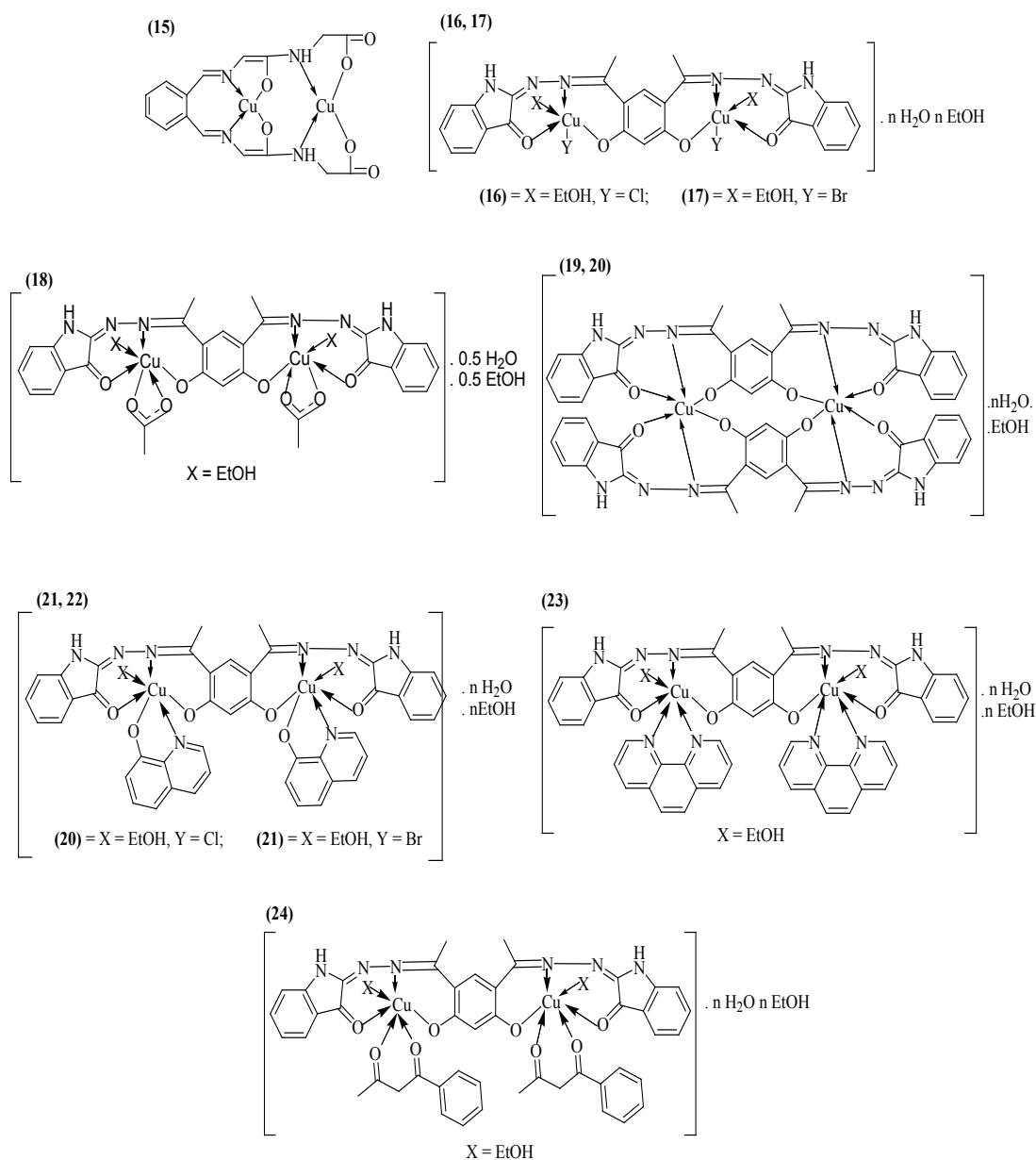
#### 4. Antibacterial Activity of Bi-nuclear Copper Complexes

Along with the synthesis of mononuclear metal complexes, a big number of binuclear metal complexes were also synthesized and have been tested for their an-

ti-microbial activities. Transition metal complexes of a copper metal ion such as [Cu<sub>2</sub>(Pym L)Cl<sub>3</sub>] on the Schiff base and Pyrimidine-derivative ligands was synthesized by template condensation of Schiff base (L) derived from glycine using 2,3-butanedione, 5-methyl-2,6-pyrimidine-dione and metal chloride/acetate salt in 1:1:2

stoichiometric ratio <sup>[17]</sup>. Synthesized compounds were well characterized by its elemental analysis, magnetic measurement and other physiochemical techniques. Tetra dentate coordination behaviour of Schiff base (L) and tridentate behaviour of 5-methyl-2,6-pyrimidine-dione (Pym) was executed by IR and NMR spectral studies. Octahedral environment surroundings of copper metal ions are revealed by UV-visible and EPR spectral studies. These structurally elucidated compounds were then screened for their antibacterial activities by taking Streptomycin as a standard reference against Gram-positive *S. aureus* and *B. subtilis* and Gram-negative *E. coli* and *S. typhi*. The Cu compound showed some excellent result

against Gram-positive bacteria and a good result against Gram negative bacteria under laboratory conditions <sup>[17]</sup>.  $[\text{Cu}(\text{NO}_3)(\text{L})]_2 \cdot \text{C}_2\text{H}_5\text{OH}$  of ligand 1-phenyl-3-methyl-4-benzoyl-5-pyrazolone-4-ethyl-thiosemicarbazone were prepared, purified and screened against Gram positive bacteria *B. cereus* and *S. aureus* and Gram negative *S. abony* using Furacilinum as the standard reference <sup>[21]</sup>. In results, the metal complexes appeared to be impactful and showed some excellent results against screened bacteria <sup>[21]</sup>. Bioactive  $[\text{Cu}_2(\text{L})(\text{H}_2\text{O})_4]$  have been synthesized with a Schiff base ligand derived from diglycine and benzene-1,2-dicarbaldehyde [Figure 1: xii (ligand); Figure 3: 15 (complex)] and evaluated for its *in vitro* antibacterial



**Figure 3.** Structure of antibacterial bimetallic copper complexes (15-24) with ligands (xii-xiii) <sup>[56-60]</sup>

activity at the concentration of  $10^3$  g/ml against *B. subtilis* and *S. aureus*, *E. coli* and *K. pneumonia* bacterial strains in the presence of three reference drugs streptomycin, ampicillin and rifampicin. The zone inhibition potential of copper complex was found much improved than free ligand<sup>[58]</sup>. Deprotonation of a potent ligand, *N,N'*-bis(*N*-hydroxyethylaminopropyl)oxamido ( $H_2heap$ ) resulted in the formation of a hydrated binuclear copper complex  $[Cu_2(heap)] \cdot (ClO_4)_2 \cdot 2H_2O$  on reaction with perchlorate salt of copper metal ion. Bioactivity of complex was evaluated against bacterial strains of *S. aureus*, *E. coli*, *B. subtilis* and recorded enhanced antibacterial potential than free ligand *in vitro*<sup>[59]</sup>. Copper complex of methoxy thiosemicarbazone (MTSC) of formulae  $[Cu(MTSC)(NH_3)_3(-Cl)] \cdot 2H_2O$  (12) and  $[Cu_2(MTSC)(NH_3)_4(Cl)_2(H_2O)_2] \cdot 2H_2O$  (13) were prepared and tested for their antibacterial potential against *B. subtilis*, *S. aureus*, *E. coli* and *P. vulgaris* with Gentamycin as reference drug. The inhibition potential data indicate that metal complexes have greater potential than free ligand<sup>[60]</sup>. 4,6-diacetylresorcinol and isatin monohydrazone yielded ligand ( $H_2L^2$ ) and then allowed to react with  $Cu^{+2}$  ion salts in 1:1 and 2:1 stoichiometric ratio resulting bioactive binuclear copper complexes [Figure 1: xii, xiii (ligands); Figure 3: 16-20 (complexes)].  $H_2L^2$  was further reacted with  $Cu^{+2}$  metal ions along with 8-hydroxyquinoline, 1,10-phenanthroline, benzoylacetone to produce mixed ligand binuclear complexes [Figure 1: ix-xi, xiii (ligands); Figure 3: 21-24 (complexes)]. *In vitro* antibacterial activity data assessment divulged that the ligands ( $H_2L^2$ ) showed activity against *S. aureus*, *B. subtilis* and *E. coli* bacteria. Complexes showed good activity against studied bacteria comparative to free ligand<sup>[56]</sup>.

## 5. Conclusions

Precisely the transitional metal complexes of copper metal ion can possess antibacterial properties as seen in the different research activities performed by a different group of people around different times. Also, it gives us hope towards achieving new heights in the field of antibacterial drugs. As we have seen during the pandemic of COVID-19, bacterial/fungal co-infections have also raised along with deadly corona virus infections and these co-infections thus increased the mortality rate in corona virus infected patients throughout the globe. The impact of readily available antibiotic drugs getting reduced by many folds because the increasing drug resistance capabilities of the bacteria, these metal complexes based drugs can help us in controlling the damage due to these deadly bacterial infections. These complexes are the hope of future medicinal chemistry as the organic-based drugs are getting ineffective against growing drug resistance of these bacteria.

The depth studies of copper coordinated metal complexes based on structural and antibacterial potential along with their synthetic route and mode of action may fulfil the future need of effective antibacterial drug for specified target microbe.

## Abbreviations

Acronym	Full word
<i>S. aureus</i>	<i>Staphylococcus aureus</i>
<i>B. subtilis</i>	<i>Bacillus subtilis</i>
<i>E. Faecalis</i>	<i>Enterococcus faecalis</i>
<i>S. mutans</i>	<i>Streptococcus mutans</i>
<i>S. gordonii</i>	<i>Streptococcus gordonii</i>
<i>B. cereus</i>	<i>Bacillus cereus</i>
<i>E. coli</i>	<i>Escherichia coli</i>
<i>S. typhi</i>	<i>Salmonella typhi</i>
<i>P. aeruginosa</i>	<i>Pseudomonas aeruginosa</i>
<i>K. pneumonia</i>	<i>Klebsiella pneumonia</i>
<i>V. cholera</i>	<i>Vibrio cholera</i>
<i>S. pneumonia</i>	<i>Streptococcus pneumonia</i>
<i>S. abony</i>	<i>Salmonella abony</i>
<i>P. mirabilis</i>	<i>Proteus mirabilis</i>
<i>S. flexneri</i>	<i>Shigella flexneri</i>
<i>M. Vaccae</i>	<i>Mycobacterium vaccae</i>
<i>S. typhimurium</i>	<i>Salmonella typhimurium</i>
<i>S. mitis</i>	<i>Streptococcus mitis</i>
<i>S. sanguinis</i>	<i>Streptococcus sanguinis</i>
<i>S. sobrinus</i>	<i>Streptococcus sobrinus</i>
<i>L. casei</i>	<i>Lactocaseibacillus casei</i>
<i>S. salivarius</i>	<i>Streptococcus salivarius</i>
<i>P. vulgaris</i>	<i>Proteus vulgaris</i>

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## Conflict of Interest

The authors declare no conflict of interest.

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